

Production of Biodiesel Through Transesterification of Crude Palm Oil (CPO) Using Montmorillonite Nanoparticles (Nano-MMT) as Heterogeneous Solid Catalyst

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Abstract—Biodiesel is an alternative energy that is environmentally friendly and has properties similar to diesel oil. One source of vegetable oil that can be used as raw material for biodiesel is Crude Palm Oil (CPO). In the CPO, there are various types of fatty acids such as palmitic acid, oleic acid, linoleic acid, stearic acid, and myristic acid. In this research, biodiesel was synthesized through the transesterification reaction of CPO using a heterogeneous solid catalyst Montmorillonite Nanoparticles (Nano-MMT). The transesterification reaction is the reaction of alcohol with triglycerides to form methyl esters (biodiesel) and glycerol with the help of an alkaline catalyst. The method used in this study was to vary the triglyceride: methanol mole ratio (1:6, 1:9, and 1:12). Through the experiment, the optimum yield of biodiesel was 84,9 grams which was obtained under reaction conditions with a catalyst weight of 4 grams, a reaction temperature of 60oC, a reaction time of 3 hours and a triglyceride: methanol mole ratio of 1:9. The best biodiesel obtained from the yield is analyzed by Gas Chromatography-Mass Spectroscopy (GC-MS). The analysis showed that the biodiesel produced contained 100% methyl ester and there were several kinds of fatty acids.

Keywords—*biodiesel, Crude Palm Oil (CPO), montmorillonite nanoparticles, heterogeneous solid catalysis, transesterification reaction*

I. INTRODUCTION

Currently the use of fuel oil in Indonesia has increased in line with the increasing population and the increasing number of vehicles. Fossil fuels are fuels used today. However, fossil fuels are natural resources that cannot be renewed so that their presence in nature is decreasing due to the increasing demands of energy needs. Solving this problem, it has been found that biodiesel production comes from biological natural sources, namely from Crude Palm Oil (CPO) from palm oil [1].

Indonesia is the second largest CPO producer in the world. This shows that CPO from palm oil has great

potential to be used as a raw material for making biodiesel in Indonesia [1].

Biodiesel is a type of biofuel that is both new and renewable [2-6]. Biodiesel (methyl ester) is formed as a result of the reaction between the ester compound (CPO) and the alcohol compound (methanol) to form a new ester compound (methyl ester) [7,8]. Biodiesel synthesis usually often uses liquid catalysts (homogeneous catalysts) yet, but the use of liquid catalysts (acid or alkaline) still has a number of obstacles, namely separating the catalyst from its products is difficult because both are in the liquid phase, corrosive, difficult to handle and store, and the remaining catalyst can no longer be used, resulting in waste that can cause environmental problems. An alternative substitute that needs to be developed is the use of solid catalysts (heterogeneous catalysts) such as Nano-Montmorillonite (Nano-MMT), because solid catalysts have several advantages, including: separation of the product is easier, handling and storage is easier, can be used repeatedly (can regenerated), as well as being more environmentally friendly [9-13].

Nano-MMT is the main content of bentonite [14,15] that has unique properties because it has a very small particle size, resulting in a very high surface area [2,13]. Besides, with a very fine size, the characteristic properties of the element will appear and can be engineered like as the properties of magnetism, optics, electricity, thermal, and others, so that their utilization has penetrated various fields of human life, such as health, information, transportation, industry, energy and catalyst [16].

This research used a transesterification reaction, which is the reaction between triglycerides and alcohol to produce methyl esters and glycerol with the help of heterogeneous solid catalyst [4,7,12,17]. The alcohol commonly used is methanol. This is because the price of methanol is cheaper and has advantages when viewed from its physical and chemical

properties, namely it is more polar and the carbon chain is shorter than ethanol [18,19] the reaction shown in **Figure 1**.

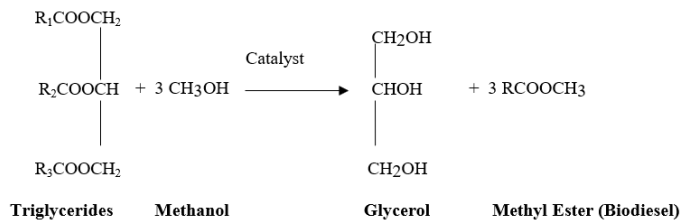


Fig. 1. Transesterification reaction.

A higher reaction rate is obtained at higher temperatures, but a reaction close to the boiling point of methanol has the potential to cause the formation of bubbles which in turn prevents the reaction at the three-phase interface (heterogeneous solid catalyst-oil-alcohol) [18]. From the results of research conducted by Nurhayati et al [1], it shows that the highest biodiesel yield is obtained at a reaction temperature of 60°C with a catalyst weight of 4% (w/w), because if the amount of catalyst is increased, the number of colliding molecules will increase and the reaction rate will also increase. However, the addition of catalyst weight to 6% and 8% (w/w) did not show an increase in biodiesel yield. The addition of excess catalyst will cause the catalyst to accumulate on the glass reactor walls and will affect the reaction balance, so that at the end of the reaction it will produce more side products.

The reaction time used is 3 hours. It is at this time that the maximum biodiesel is produced. In the initial stage of the transesterification was rapid reaction rate, and then the speed decreases and finally reaches equilibrium in about 3 hours. It can be explained that the transesterification reaction between oil and alcohol is reversible, when the reaction time is long enough. The length of the reaction time depends on the conditions of the oil used. Oils with a large amount of free fatty acids and water require a longer reaction time than oils with small amounts of free fatty acids and water [1].

Research on the transesterification reaction of CPO with temperature, reaction time, and weight of solid catalyst which was still micro-sized in previous research by Nurhayati et al [1] has been carried out. However, the researchers used Nano-MMT as heterogeneous solid catalyst using a variation of stoichiometric ratios for the transesterification reaction to produces 100% biodiesel yield.

II. MATERIALS AND METHODS

A. Tools and Materials

The equipment used were a furnace, sieve, desiccator, porcelain cup, oven, analytical balance, magnetic stirrer hotplate, thermometer, three-neck flask complete with condenser, magnetic stirrer, separating funnel, Whatman 42 filter paper, stopwatch, and equipment other glasses commonly used in laboratories.

The materials used in this study were nano-montmorillonite, CPO, and methanol.

B. Preparation and Characterization of Nano-MMT as Heterogeneous Solid Catalysts

Synthesis of Nano-MMT material, which is top-down where the synthesis of nano-sized particles directly reduces large materials by grinding with a milling tool, where Montmorillonite is milled with a High Energy Milling (HEM) tool with a milling time of 15 minutes and then characterized with Particles Size Analyzer (PSA).

C. Biodiesel Production Through Transesterification Reaction with Nano-MMT as a Catalyst Using the Mole Ratio of CPO: Methanol (1: 6, 1: 9, and 1:12)

- Prepared a three-neck round flask and connected to a condenser (reflux condenser circuit) equipped with a magnetic stirrer and a thermometer.
- Prepared 4 grams of Nano-MMT heterogeneous solid catalyst and 23.82 g of methanol (1: 6), then mix the two ingredients and stirrer for 10 minutes, and prepared 100 grams of CPO (50°C) then put the mixture into a round three neck flask to refluxed for 3 hours at 250 rpm at temperatures 60°C.
- Moved the reflux product to a separating funnel and left at room temperature until 2 layers are formed, where the top layer is biodiesel and the bottom layer is glycerol, furthermore separated.
- Washed biodiesel with clean water (55°C), separated the biodiesel from water, filtered with whatman 42 paper and measure the weight of biodiesel.
- Repetition of treatment was carried out for variations in the mole ratio of CPO: methanol (1: 9 and 1:12) with the same Nano-MMT catalyst weight of 4 grams.
- The biodiesel produced was analyzed using GC-MS.

D. Biodiesel Analysis Using Gas Chromatography Mass Spectrometry (GC-MS)

Analysis on biodiesel testing on CPO was carried out using GC-MS which expressed in two parameters, specifically retention time (minutes) and concentration (%). The retention time is a specific number of interactions between compound molecules in the chromatography column. It is a qualitative indicator of the compound under certain conditions, and the concentration shows the level of purity of the analyzed sample.

III. RESULTS AND DISCUSSION

A. Results of Nano-MMT Characterization Using PSA

Montmorillonite which has been milled for 15 minutes and characterized using PSA produces Nano-MMT with a smallest distribution size of 17.7 nm as shown in **Figure 2**. The Nano-

MMT is then used as heterogeneous solid catalyst in making biodiesel by transesterification of CPO.

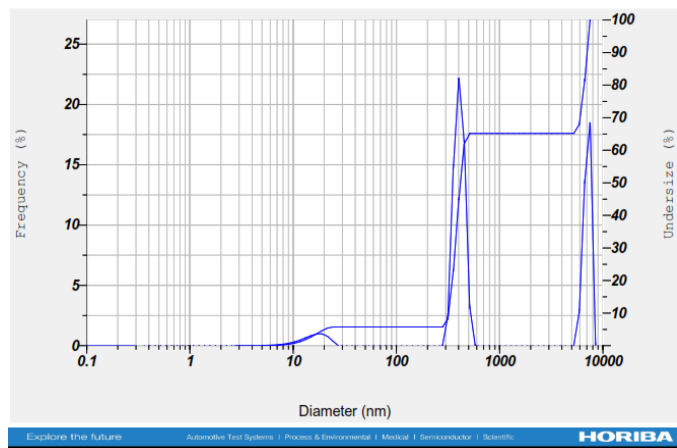
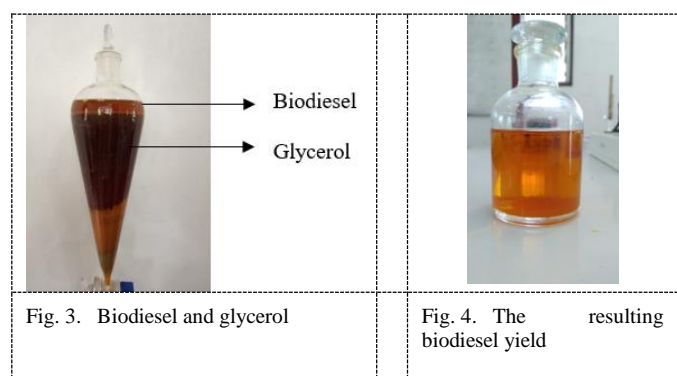


Fig. 2. Montmorillonite Distribution Number chart with 15 minutes milling time.

B. Effect of the molar ratio of CPO: Methanol

The biodiesel and glycerol formed can be shown in **Figure 3** where the top layer is biodiesel and the bottom layer is glycerol. The resulting biodiesel yield as shown in **Figure 4** is strongly influenced by the molar ratio of alcohol to triglycerides. The stoichiometric ratio for transesterification requires three moles of alcohol and one mole of triglycerides to produce three moles of fatty acid esters and one mole of glycerol. Transesterification requires a large excess of alcohol to drive the reaction to the right. However, too high molar ratio of alcohol to vegetable oil causes an increase in the solubility of glycerol in the methyl ester layer which makes the separation process difficult [5].



Increasing the mole ratio of CPO: methanol from 1: 6 to 1: 9 increased the yield of biodiesel from 39% to 84.9%. Furthermore, the molar ratio of CPO: methanol could not increase the yield of biodiesel than before. This is due to the excess or lack of methanol will only result in an increase in the formation of glycerol and emulsion. That means, glycerol will dissolve in excess methanol and then inhibits the methanol

reaction in the catalyst reactant, thereby disrupting the separation of glycerol [1]. Furthermore, based on the result of this research the optimum yield of biodiesel was 84,9 grams which was obtained under reaction conditions with a catalyst weight of 4 grams, a reaction temperature of 60°C, a reaction time of 3 hours and a triglyceride: methanol mole ratio of 1:9 as shown in the **Figure 5**.

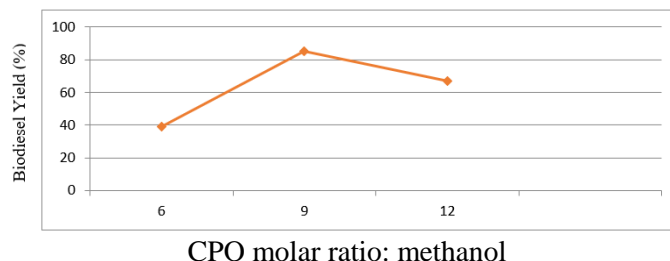


Fig. 5. Effect of CPO: Methanol molar ratio on biodiesel yield.

C. Results of Biodiesel Analysis Using GC-MS

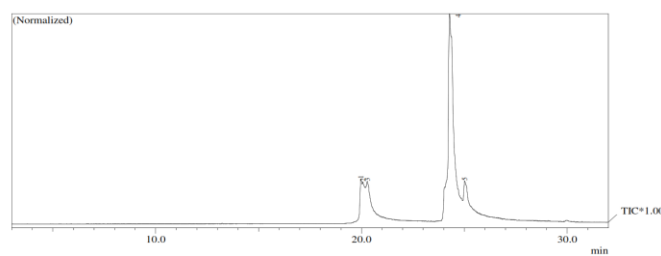


Fig. 6. Peak GC of Biodiesel.

TABLE I. PEAK REPORT TIC OF GAS CHROMATOGRAPHY ANALYSIS FOR BIODIESEL PRODUCTS

| Peak | R.Time (min) | Area | Area (%) | Name |
|------|--------------|----------|----------|--|
| 1 | 19.971 | 801186 | 4.73 | Hexadecanoic acid, methyl ester \$ Palmitic acid, methyl ester \$ Hexadecanoic acid methyl |
| 2 | 20.071 | 997399 | 5.89 | Hexadecanoic acid, methyl ester (CAS) Methyl palmitate \$ Methyl hexadecanoate |
| 3 | 20.282 | 1799124 | 10.62 | Hexadecanoic acid, methyl ester (CAS) Methyl palmitate \$ Methyl hexadecanoate |
| 4 | 24.281 | 11564050 | 68.23 | 9-Octadecenoic acid (Z)-, methyl ester (CAS) Methyl oleate \$ Oleic acid methyl ester |
| 5 | 25.017 | 1786380 | 10.54 | Cyclopentanetri-decanoic acid, methyl ester (CAS) Methyl dihydrochaulmoograte |
| | | 16948139 | 100.00 | |

Based on the result of GC-MS analysis of biodiesel produced five kinds of chromatogram peaks in which there are types of methyl esters which can be seen in the **Figure 6**. It was showed that the biodiesel produced contained 100%

methyl ester and there were several kinds of fatty acids. Furthermore, the fourth peak has the largest percentage area of 68.23% as shown in the **Table 1**. Where according to SNI 04-7182-2006 these results have met the quality standard requirements for biodiesel with a minimum ester content of 96.5%.

IV. CONCLUSION

The results publicized that the optimum biodiesel yield of 100 g of CPO is 84.9% obtained under the following reaction conditions: 4% catalyst (w/w), 60°C reaction temperature, 3 hours reaction time and 1: 9 molar ratio of CPO: methanol. The biodiesel produced in this study has met the SNI 04-7182-2006 biodiesel quality standard which is shown from the GC-MS analysis that the biodiesel product produced has an ester content of 100%.

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