



Experimental Study on Re grinding Flotation of a Gold Mine in Gansu Province

Yanbo Chen^{1,*}, Guangsheng Li¹, Wenwen Meng³, Xingfu Zhu¹, Junjie Wang¹,
Kun Song²

¹Selection and metallurgy laboratory of Shandong Gold Mining Technology Co. Ltd., Yantai, Shandong, 261441, China

²Xihe County Zhongbao Mining Co., Ltd., Longnan, Gansu, 742100, China

³Shandong Gold Group Technology and Environmental Protection Center, Jinan, Shandong, 742100, China.

*595907901@163.com

Abstract. The gold mineral in a difficult to select gold mine has a relatively fine particle size, with an average particle size of 3.58 μ m. Mainly in the form of fine-grained embedding. The main gold bearing mineral is pyrite, with an average particle size of 32.80 μ m. 20 μ The content of particles below m is 33.84%, and the content of fine particles is relatively high. Due to the fine particle size of gold ore and gold bearing mineral pyrite, it belongs to difficult to select gold ore. The flotation recovery rate of conventional beneficiation process is about 80%. In order to further improve the flotation recovery rate of this difficult to select gold mine, experimental studies were conducted on the "intermediate ore re grinding flotation" and "intermediate ore coarse particle re grinding flotation" of the flotation intermediate ore, and based on the experimental research, on-site process flow transformation measures were proposed.

Keywords: Difficult to select gold mines; Re grinding; flotation.

1 Introduction

A certain gold mine beneficiation plant adopts a one-stage grinding process, and the grinding fineness of the selected raw ore is controlled at around -200 mesh 75%. Due to the fact that the pyrite, which is the main gold bearing mineral in the selected raw ore, is distributed in a fine-micron particle pattern (with an average particle size of 32.80 μ m) A stage of grinding cannot achieve sufficient dissociation of pyrite, which affects the gold grade and recovery rate of flotation concentrate. However, adding a grinding section (requiring the addition of a ball mill) not only increases equipment investment and energy consumption, but also occupies the already limited factory space. In order to further improve the gold grade and recovery rate of flotation concentrate, reduce the occupation of factory space, and reduce equipment investment and energy consumption, a re grinding experiment was carried out for flotation intermediate ore (the amount of ore selected in flotation is significantly reduced compared to the original ore,

© The Author(s) 2024

A. E. Abomohra et al. (eds.), *Proceedings of the 2023 9th International Conference on Advances in Energy Resources and Environment Engineering (ICAESSEE 2023)*, Atlantis Highlights in Engineering 29,

https://doi.org/10.2991/978-94-6463-415-0_54

achieving precise grinding of pyrite continuous body, reducing equipment investment and grinding process energy consumption), to determine the feasibility of re grinding flotation intermediate ore and the re grinding process. For this purpose, experimental studies were conducted on the "intermediate ore regrinding flotation" and "intermediate ore coarse particle regrinding flotation" of flotation intermediate ores provided on the production site. The results showed that the recovery rate of "coarse particle regrinding flotation" after mixing six flotation intermediate ores (equivalent to full particle size) was 21.80% higher than that of unground, which was higher than the recovery rate of direct regrinding flotation after mixing one, two, three, one, and two fine tailings (5.87%). Based on this, a transformation measure of "intermediate ore classification coarse particle separate re grinding flotation" is proposed.[1-3]

2 Sample analysis

Perform laboratory analysis on the incoming samples, and the results are shown in Table 1.

Table 1. Test and analysis results

Sample name	Gold grade/(g/t)	Sulfur grade/%
Flotation concentrate	24.38	35.54
Primary cleaner tailing	5.64	6.44
Secondary cleaner tailing	6.68	8.42
Thirdly cleaner tailing	13.35	18.25
Primary scavenger concentrate	5.01	4.39
Secondary scavenger concentrate	3.84	4.01
Thirdly scavenger concentrate	3.18	3.29
Flotation tailings	0.45	0.21

3 Particle size sieving analysis

Particle size analysis was performed on 8 samples including concentrate, with a focus on examining three particle sizes: +100 mesh, -100+200 mesh, and -325 mesh. The results are shown in Tables 2.

Table 2. Sample+100 mesh sieve analysis results

Sample name	Yield/%	Gold grade/(g/t)	Au distribution rate/%	Sulfur grade/%	Sulfur distribution rate/%
Flotation concentrate	0	0	0	0	0
Primary cleaner tailing	11.95	5.92	12.53	4.1	7.61
Secondary cleaner tailing	12.71	6.19	11.78	3.72	5.62
Thirdly cleaner tailing	12.08	13.76	12.45	7.14	4.73
Primary scavenger concentrate	12	5.17	12.38	3.86	10.88
Secondary scavenger concentrate	10.44	4.16	11.32	4.26	11.09
Thirdly scavenger concentrate	8.79	4.42	12.22	2.68	7.16
Flotation tailings	5.31	0.71	8.38	0.28	7.24

Ten test samples were screened using a standard sieve for particle size analysis. The screening results showed that the +100 mesh particle size content in the flotation concentrate (three fine tailings and three sweeping concentrates) was about 10%, and the gold distribution rate was about 12%. However, the +100 mesh particle size content in the concentrate was zero, indicating that all 12% of the +100 mesh gold in the flotation concentrate did not enter the concentrate. Therefore, it is necessary to conduct experimental research on coarse particle size re grinding and flotation of the flotation concentrate.

4 Experimental study^[4-7]

4.1 Flotation Middling regrinding - flotation test

Six flotation samples were finely ground and then subjected to roughing. The changes in gold grade and recovery rate of the flotation concentrate were examined to determine the suitable samples for re grinding flotation treatment and the grinding fineness. The experimental process and conditions are shown in Figure 1.

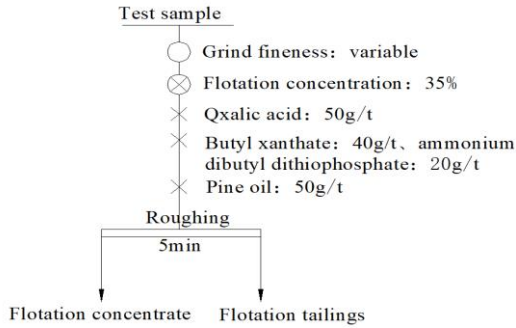


Fig. 1. Test Process

Table 3. Test Results

Sample name	Optimal grinding fineness(-200 mesh)/%	Unground ore sample flotation concentrate		Flotation concentrate under optimal grinding fineness conditions	
		Gold grade/(g/t)	Rate of recovery/%	Gold grade/(g/t)	Rate of recovery/%
Primary cleaner tailing	67	5.89	90.69	7.23	93.87
Secondary cleaner tailing	65	7.10	92.16	8.18	94.98
Thirdly cleaner tailing	58	13.92	97.77	15.15	97.59
Flotation Mid-dling Primary scavenger concentrate	82	5.36	86.63	7.41	90.03
Secondary scavenger concentrate	71	4.54	80.73	5.17	87.99
Thirdly scavenger concentrate	65	4.08	79.15	4.21	89.64
Mixed Flotation Mid-dling Scavenger concentrate+Primary cleaner tailing+Secondary cleaner tailing	76	4.99	84.33	6.23	88.3
66	6.92	84.17	7.97	90.04	

According to Table 3, except for the refined three tailings, the gold grade and recovery rate of the flotation concentrate after regrinding in the other five flotation processes have all been improved to varying degrees. Considering that in the actual production process, the flotation concentrate should be mixed before regrinding, and the first, second, and third concentrates should be mixed in a certain proportion before grinding flotation treatment. When the grinding fineness is -200 mesh and the content is 76%, the flotation recovery rate is 3.97% higher than that without grinding. Mix the first, second, third, first, and second tailings in a certain proportion before grinding. When the grinding fineness is -200 mesh and the content is 66%, the flotation is 5.87%

higher than that without grinding. Compared to the two, the recovery rate of grinding flotation after mixing the first, second, third, first, and second tailings is higher.

4.2 Coarse particle regrinding flotation test of Flotation Middling

Use a standard sieve to screen out the ore with a particle size of 200 mesh or more from six flotation tailings, namely, sweeping one fine, sweeping two fine, sweeping three fine, sweeping one fine, sweeping two fine, and sweeping three fine. Conduct further grinding flotation tests on the coarse particle size of 200 mesh or more to examine the changes in gold grade and recovery rate of the flotation concentrate. The experimental process and conditions are shown in Figure 2.

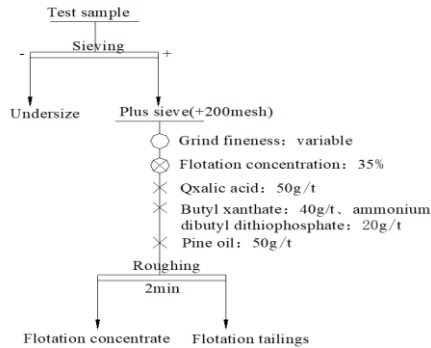


Fig. 2. Test Process

Table 4. Test Results

Sample name	Optimal grinding fineness(-200mesh)/%	Unground ore sample flotation concentrate		Flotation concentrate under optimal grinding fineness conditions		
		Gold grade/(g/t)	Rate of recovery/%	Gold grade/(g/t)	Rate of recovery/%	
Flotation Middling(+200mesh)	Primary cleaner tailing	54	5.87	32.56	8.11	69.05
	Secondary cleaner tailing	53	7.48	36.17	9.33	79.43
	Thirdly cleaner tailing	51	14.31	49.31	18.85	82.68
	Primary scavenger concentrate	50	5.23	25.78	6.9	58.98
	Secondary scavenger concentrate	48	4.77	32.9	6.45	65.23
	Thirdly scavenger concentrate	72	4.54	27.52	7.78	55.34
Mixed Flotation Middling(+200mesh)	Cleaner tailing+Scavenger concentrate	51	6.74	31.7	10.6	74.91

According to Table 4, it can be seen that the recovery rates of the flotation concentrate after coarse particle re-grinding of the six flotation Middlings have been improved to varying degrees, and are all higher than the recovery rates of the direct re-grinding flotation of the six Middlings. The recovery rate of "coarse particle re-grinding flotation" after mixing six flotation samples increased by 43.21% compared to ungrounded samples. Comparative experiments under different reaction time.

5 Conclusion

The experimental research results show that the gold grade of the flotation concentrate increased by 3.86g/t and the recovery rate (equivalent to the full particle size) increased by 21.80% after the coarse grade re-grinding of the flotation intermediate ore (sweeping and finishing), which is much higher than the gold grade of 1.05g/t and the recovery rate of 5.87% after the mixed intermediate ore re-grinding. In addition, only re-grinding coarse particles can significantly reduce the amount of re-grinding and avoid interference and over-grinding of fine particles. Therefore, the "coarse particle re-grinding flotation" treatment method is suitable for medium ore.

References

1. Kangying BI, et al.: Experimental Study on Re-grinding of Lead Concentrate in a Certain Lead Zinc Sulfide Mine. *Modern Mining*(5),145-148(2023).
2. Jianwei YANG, et al.: Experimental Study on Fine Grinding and Re-selection of Flotation in a Gold Mine in Gansu Province. *Xinjiang Nonferrous Metals*(2),51-53(2022).
3. Jinjin WANG, et al.: Research and production practice on the re-grinding process of tin copper sulfide ore. *Yunnan Metallurgy* 46(3),19-26(2017).
4. Xizhen YUAN, et al.: A Study on Improving Copper Recovery by Re-grinding and Re-selection of Ore and Tailings in Flotation of a Mixed Mine. *Copper Engineering* (1), 34-39(2021).
5. Zhensheng JIANG, et al.: Experimental study on improving the recovery rate of low-grade phosphate ore through secondary grinding of Zhongkuang. *Industrial Minerals & Processing* (10),4-6(2013).
6. Bayat O, Ucurum M, Poole C. Effects of size distribution on flotation kinetics of Turkish sphalerite[J]. *Mineral Processing & Extractive Metallurgy Imm Transactions*, 113 (113): 53-59(2013).
7. Bradshaw D J, Buswell A M, Harris P J, et al:Interactive Effects of the Type of Milling Media and Copper Sulphate Addition on the Flotation Performance of Sulphide Minerals from Merensky Ore Part I:Pulp Chemistry[J].*International Journal of Mineral Processing*,78(3):153-163(2006).

Open Access This chapter is licensed under the terms of the Creative Commons Attribution-NonCommercial 4.0 International License (<http://creativecommons.org/licenses/by-nc/4.0/>), which permits any noncommercial use, sharing, adaptation, distribution and reproduction in any medium or format, as long as you give appropriate credit to the original author(s) and the source, provide a link to the Creative Commons license and indicate if changes were made.

The images or other third party material in this chapter are included in the chapter's Creative Commons license, unless indicated otherwise in a credit line to the material. If material is not included in the chapter's Creative Commons license and your intended use is not permitted by statutory regulation or exceeds the permitted use, you will need to obtain permission directly from the copyright holder.

