

Removal of fluoride from aqueous solution by adsorption on lanthanum modified attapulgite

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Abstract—Fluoride pollution in natural water may create severe threats for human health. In this study, lanthanum modified attapulgite (La-ATP) was synthesized and used as a novel adsorbent for removal of fluoride in aqueous solution. Characterized results showed that the mass content of Lanthanum oxide was 3.30%. La-ATP exhibited high adsorption affinity for aqueous fluoride and the maximum adsorption amounts were 16.92, 22.03 and 25.91 mg/g at 15, 25 and 35 °C, respectively. Adsorption kinetic followed pseudo-second kinetics model and adsorption rates decreased with increasing initial concentration of fluoride. The amount adsorbed of fluoride onto La-ATP decreased generally with increasing solution pH. The presence of coexisted anions in water decreased the adsorption amount of fluoride by competitive adsorption. Fluoride loaded La-ATP can be easily desorbed in alkaline solution and the regenerated adsorbent still possessed high adsorption capacity for aqueous fluoride. The results implied that La-ATP may be an efficient adsorbent for the removal of aqueous fluoride.

Keywords- Lanthanum modified attapulgite; adsorption; desorption; fluoride

I. INTRODUCTION

Fluoride pollution in the environment can occur due to natural sources and anthropogenic sources [1]. Fluoride frequently exists in minerals and it can be leached out due to erosion by rainwater, thereby allowing it to contaminate ground and surface water. On the other hand, fluorine compounds are industrially important and are extensively used in glass and semiconductors manufacturing, fertilizers operation, steel and aluminum industries, and nuclear applications [2]. Fluoride is one of the essential trace elements for human body [3]. Excess fluoride in drinking water causes harmful effects such as dental and skeletal fluorosis [4]. The presence of fluorine in drinking water is beneficial to the production and maintenance of healthy bones and teeth when its content is within permissible limits [3]. Long term ingestion of high fluoride drinking water may cause dental or skeletal fluorosis [5]. The World Health Organization has set a guidance value of 1.5 mg/L for fluoride in drinking water [6, 7]. China also adopted 1.0 mg/L as the upper limit.

Various methods such as chemical precipitation [8], ion exchange [9], electrodialysis and electrolysis [10, 11], and adsorption [12] were developed to remove fluorides in aqueous solution. Among these methods, adsorption is still an effective and one of the most suitable methods for

defluoride of water because it is economical, environmentally benign and efficient [13, 14]. In recent years, many adsorbents have been reported to be effective for removal of aqueous fluoride, such as activated carbon [14], alumina and its composites [15, 16], fly ash [13, 17], clay minerals [18, 19], chitosan [20], resins [21], and so on. Among these, clay mineral adsorbents have received great attention because they are natural, inexpensive.

Attapulgite (ATP) is a kind of crystalline hydrated magnesium aluminum silicate mineral, which has been extensively used as adsorbents to remove the organic and inorganic pollutants because of its porous structure, high surface area and low cost [22]. However, removal of fluoride from aqueous solution by adsorption onto attapulgite is very limited. Numerous studies have shown that lanthanum-based adsorbents, such as La-incorporated chitosan beads [23], La-resin [24], La loaded natural zeolite [25], lanthanum-impregnated silica gel [26], have a high affinity for fluoride in aqueous solution. Therefore, lanthanum modified attapulgite (La-ATP) may improve the adsorption capacity for fluoride. To our best knowledge, no efforts have been made to develop lanthanum modified attapulgite to remove the aqueous fluoride.

In this study, lanthanum modified attapulgite were prepared and used as a novel adsorbent for the removal of fluoride. Adsorption and desorption behaviors of aqueous fluoride on La-ATP were studied by batch experiments. Effect of solution chemistry properties such as solution pH and competitive anions on fluoride adsorption was also described.

II. EXPERIMENTAL

A. Materials

Attapulgite (100 mesh) was purchased from HuiDa Mining Technology Co., Ltd., Jiangsu, China. Lanthanum(III) nitrate ($\text{La}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$) and other reagents of analytical grade were obtained from Sinopharm Chemical Reagent Co., Ltd., Shanghai, China.

B. Preparation of adsorbent

Typically, 10 g attapulgite powder was dispersed in 150 ml deionised water, and was sonicated at a power setting of 300 W for 20 min. After settling for a few minutes, the bottom sediment is drained, followed by filtering and drying. Five grams treated attapulgite were dispersed in 100 ml hydrochloric acid of 1 mol/L, and the

mixture was stirred magnetically for 2 h at room temperature. The solid was filtrated and washed deionized water until pH 6, and dried at 100 °C at vacuum drying chamber. The resulting solid was referred as HCl-attapulgit.

Five milligram of HCl-attapulgit and 0.94 g $\text{La}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ was dispensed in 200 mL deionised water. Complete dispersion of the clay was achieved by stirring the slurry at the room temperature for 2 h. The mixture was kept in 80 oC under constant stirring for 48 h, followed by filtering and washing with deionised water, then dried at vacuum drying oven and calcinated at 300 oC for 2 h. Then lanthanum modified attapulgit (La-ATP) was obtained.

C. Characterization of La-ATP

The mineralogical and chemical compositions of natural attapulgit and La-ATP were determined by X-ray fluorescence (XRF, Eval).

D. Adsorption experiment

A stock solution containing 1000 mg/L fluoride was prepared by dissolving appropriate amount of sodium fluoride in double distilled water. Experimental solutions for adsorption and analysis were then prepared freshly by diluting the stock solution. Typically, 20 mg of La-ATP was added to 40 ml of fluoride solution with pH 6.0 and the initial concentration in the range of 5~60 mg/L. The suspensions were mixed in incubator shaker at 15, 25, and 35 °C and shaken for 4 h. After reaching adsorption equilibrium, the solution was filtered through 0.45 µm membrane and the filtrate was analyzed for residual fluoride concentration by ion selective electrode [27]. The adsorption amount of fluoride on La-ATP was calculated using the following equation:

$$q_e = \frac{(C_0 - C_e) \cdot V}{W} \quad (1)$$

Where C_0 (mg/L) is the initial concentration of fluoride, C_e (mg/L) is the equilibrium concentration of fluoride, V (L) is the volume of solution, and W (g) is the weight of La-ATP.

For adsorption kinetics experiments at 25 °C, 200 mg La-ATP was added into 400 ml fluoride solution at pH value of 6.0 and initial concentration of 10, 30, and 50 mg/L, respectively under strong magnetic stirring. At selected time periods, a certain amount of sample was withdrawn from the flask and filtrated. The residual fluoride concentration in solution was determined by ion selective electrode.

The pH effect on fluoride adsorption was investigated in a pH range from 3 to 11. a series of glass tubes receiving 20 mg La-ATP and 40 ml of 50 mg/L fluoride solution was pre-adjusted to the desired pH value by 0.1 mol/L HCl or 0.1 mol/L NaOH and shaken at 25 °C for 4 h. Effect of competitive ions on fluoride adsorption was studied by dispersing 20 mg La-ATP in 40 ml of NaCl, NaNO_3 , Na_2SO_4 , or Na_2CO_3 solution (5–25 mmol/L) containing 50 mg/L fluoride at pH 6.0 and 25 °C.

E. Desorption and regeneration

To examine the desorption property of fluoride from La-ATP adsorbent, 100 mg La-ATP was placed into 40 ml of 50 mg/L fluoride solution. After fluoride adsorption

at pH 6.0 and 25 °C for 4 h, fluoride loaded La-ATP was separated centrifugally and regenerated in 25 ml of 0.1 mol/L NaOH solution for 2 h. Then regenerated La-ATP was separated centrifugally and washed with deionized water for three times to remove any unadsorbed fluoride. The adsorption and regeneration experiments were followed for 4 cycles.

III. RESULTS AND DISCUSSION

A. Adsorbent characterization

The chemical composition of ATP and La-ATP characterized by X-ray fluorescence analyses were tabulated in Table 1. From the results, the attapulgit was successfully modified by lanthunum and the mass content of La_2O_3 was 3.30%. And also, the mass content of MgO , Fe_2O_3 , CaO and Al_2O_3 , was degraded. This may be

Sample	wt%					
	SiO_2	Al_2O_3	MgO	Fe_2O_3	CaO	TiO_2
ATP	64.5	13.9	7.54	8.44	0.19	1.65
La-ATP	63.3	13.4	6.16	8.24	0.06	1.58
	MnO	K_2O	Na_2O	La_2O_3	SO_3	CO_2
ATP	0.11	2.39	0.13	---	0.02	1.06
La-ATP	0.07	2.23	0.13	3.30	0.04	1.17

probably because that the attapulgit consists of a typical unit cell with Mg, Fe, Ca and Al cations that can be easily exchanged. Lanthanum ions may replace the cations such as Mg, Fe, Ca and Al.

TABLE 1 THE CHEMICAL COMPOSITION OF ATP AND LA-ATP

B. Adsorption isotherms

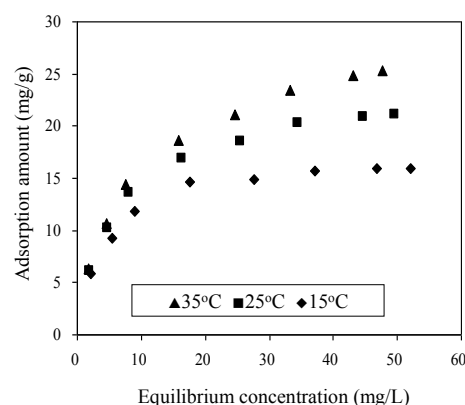


Figure 1. Adsorption isotherms of fluoride onto La-ATP at 15, 25, and 35 °C.

TABLE 2 LANGMUIR AND FREUNDLICH ADSORPTION MODEL PARAMETERS OF FLUORIDE ADSORPTION ON La-ATP AT 15, 25 AND 35°C

T (°C)	Langmuir model			Freundlich model		
	$q_m(\text{mg/g})$	b (L/mg)	R^2	n	K_f	R^2
15	16.92	0.26	0.99	3.38	5.46	0.92
25	22.03	0.20	0.99	2.73	5.53	0.96
35	25.91	0.17	0.99	2.43	5.55	0.97

Adsorption isotherms of fluoride onto La-ATP at 15, 25, 35 °C were illustrated in Fig .1. From the results, fluoride adsorption amount increased with the increase of equilibrium concentration of fluoride in solution. To further verify the fluoride adsorption mechanism, Langmuir model and Freundlich models were used to fit the experimental data. Langmuir model can be expressed as:

Langmuir model:

$$\frac{1}{q_e} = \frac{1}{q_m} + \frac{1}{q_m b C_e} \quad (1)$$

Freundlich model:

$$\log q_e = \log K_f + \frac{1}{n} \log C_e \quad (2)$$

Where q_e (mg/g) is the equilibrium amount adsorbed, C_e (mg/L) is the equilibrium concentration of fluoride, q_m (mg/g) is the theoretical capacity adsorbed of fluoride, b (L/mg) is the affinity coefficient, K_f ($\text{mg}^{1-1/n} \cdot \text{L}^{1/n}/\text{g}$) is Freundlich constant and $1/n$ is the heterogeneity factor.

Simulated parameters of adsorption isotherms by Langmuir and Freundlich model were compiled in Table 2. At 15, 25 and 35°C, the correlation factors (R^2) based on Langmuir model ($R^2 > 0.99$) is higher than Freundlich model ($R^2 < 0.97$). The calculated adsorption capacity from Langmuir model is almost identical to the experimental data. Therefore, Langmuir model can fit adsorption isotherms of fluoride onto La-ATP very well, indicating of monolayer adsorption. The maximum adsorption capacity at 15, 25, and 35 °C is 16.92, 22.03 and 25.91 mg/g, respectively.

C. Adsorption kinetics

The adsorption kinetics of fluoride onto La-ATP at the initial fluoride concentrations of 10, 30 and 50 mg/L are compiled in Fig. 2. From the kinetics curves, the adsorption of fluoride was quickly in the first 10 min and reached the adsorption equilibrium completely within 60 min. To further describe experimental data, pseudo-first-order and pseudo-second-order model were tested to fit the experimental kinetics data. The pseudo-first-order kinetics model is given as:

$$\log(q_e - q_t) = \log q_e - \frac{k_1}{2.303} t \quad (3)$$

The pseudo-second-order kinetics model is expressed as:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \quad (4)$$

Where q_e is the equilibrium adsorption amount, mg/g, q_t is the adsorption amount at time t , mg/g and k_1 , k_2 is pseudo-first-order and pseudo-second-order rate constant, respectively.

The simulated results are given in Table 3. For pseudo-first-order model, the value of correlation coefficient (R^2) is extremely low and the calculated equilibrium amount is far from the experimental values, which indicate that adsorption of fluoride onto La-ATP can not follow the pseudo-first-order kinetic model. But for pseudo-second-order kinetics, the correlation coefficient is relatively high ($R^2 > 0.999$) and the equilibrium adsorption capacity determined by using pseudo-second order model is nearly identical with the experimental results, suggesting that fluoride adsorption onto La-ATP can be fitted by pseudo-second-order kinetics model. In addition, the rate constants of fluoride onto La-ATP decreased with increasing initial concentration, indicating of a rapid uptake rate at lower initial concentration. This may be because fluoride molecules in solution can easily find the available groups of La-ATP and attach instantly to the adsorbent surface at lower initial fluoride concentration. However, at higher initial concentration, a larger number of fluoride molecules are adsorbed on the surface of La-ATP and occupy most of active adsorption sites. Fluoride

molecules to be further adsorbed must overcome the electrostatic repulsion with fluoride molecules in solution and find available adsorption sites on the surface of La-ATP, thus lead to a low adsorption rate.

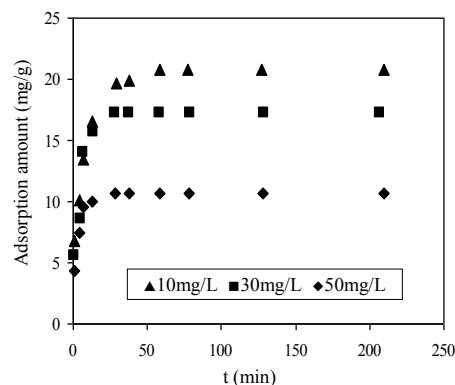


Figure 2. Adsorption kinetics of fluoride onto La-ATP at initial concentration of 10, 30, and 50 mg/L.

TABLE 3. SIMULATED RESULTS OF FLUORIDE ONTO LA-ATP USING PSEUDO-FIRST ORDER AND PSEUDO-SECOND ORDER KINETICS

C_0 mg/L	q_e mg/g	Pseudo-first order kinetics			Pseudo-second order kinetics		
		k_1 1/min	q_{cal} mg/g	R^2	k_2 g/(mg·min)	q_{cal} mg/g	R^2
10	10.67	1.9×10^{-1}	6.61	0.90	1.0×10^{-1}	10.74	0.999
30	17.26	1.7×10^{-1}	14.59	0.92	3.2×10^{-2}	17.51	0.999
50	20.81	8.9×10^{-2}	14.64	0.98	1.6×10^{-2}	21.23	0.999

D. Effect of solution pH

The effect of pH on fluoride removal from aqueous solution by La-ATP was studied at various pH values (ranging from 3 to 11). As illustrated in Fig. 3, it is apparent that solution pH has significant effect on adsorption capacity and Adsorption amount of fluoride decreased monotonously with an increase of solution pH. Under acidic conditions, due to protonation, adsorbent surface is positively charged, which is conducive to the adsorption of fluoride. Under alkaline conditions, lower adsorption amount which may be attributed to unfavorable surface charges and competition for adsorption sites due to excess anions at alkaline conditions.

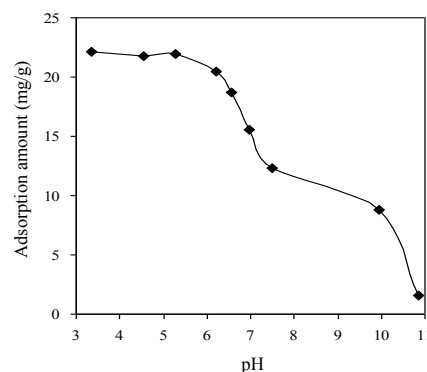


Figure 3. Effect of solution pH on F^- adsorption on La-ATP

E. Effect of competitive ions

Drinking water and wastewater contains many competitive anions. Therefore, it was necessary to study the effect of competitive ions such as Cl^- , NO_3^- , SO_4^{2-} , and CO_3^{2-} , on the adsorption of fluoride onto La-ATP [28]. The

results were given in Fig. 4. It is clear that the presence of Cl^- , NO_3^- , SO_4^{2-} , and CO_3^{2-} reduces adsorption of fluoride, and adsorption amount of fluoride decreased gradually with increasing anions concentration, which indicates that the presence of anions such as Cl^- , NO_3^- , SO_4^{2-} , and CO_3^{2-} may compete with F^- in solution and decrease the adsorption of fluoride onto La-ATP. The anions reduced the fluoride adsorption in the order was $\text{CO}_3^{2-} > \text{SO}_4^{2-} > \text{Cl}^- > \text{NO}_3^-$. The anions CO_3^{2-} showed the greatest impact for the adsorption of fluoride. This may be attributed to the change of solution pH as well as the competing effect of these co-anions after the addition of competitive ions.

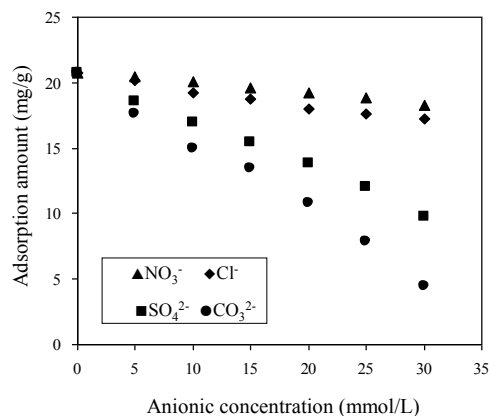


Figure 4. Effect of competitive ions on fluoride adsorption onto La-ATP.

F. Desorption and regeneration

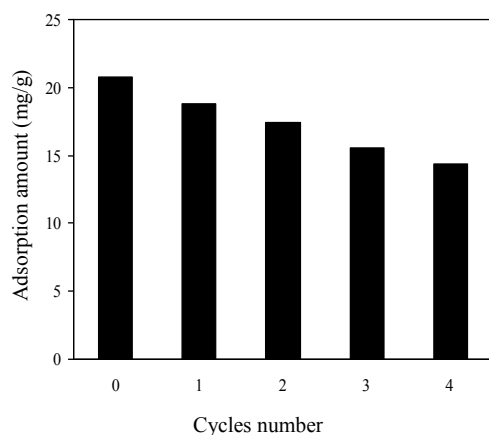


Figure 5. Desorption and regeneration histogram of fluoride onto La-ATP.

From the results of Fig. 3, the lower adsorption amount of fluoride on La-ATP at higher pH implied that fluoride loaded La-ATP can be desorbed in alkaline solution. Desorption and regeneration experiments used 0.1 mol/L NaOH solution. The results of desorption and regeneration were shown in Fig. 5. It was observed that adsorption amount of fluoride onto La-ATP decreased from 20.77 mg/g to 18.78 mg/g in the first adsorption-regeneration cycle. And adsorption amount was 14.38 mg/g after four desorption-regeneration cycles. This result indicates that the regenerated La-ATP still possessed high adsorption capacity and had a good recycling ability.

IV. CONCLUSION

Lanthanum modified attapulgite was prepared and used for the adsorptive removal of fluoride in aqueous solution.

Fluoride adsorption can be fitted very well by Langmuir model and the adsorption capacity increase with adsorption temperature. Adsorption kinetics follow pseudo-second kinetic model and the adsorption rates decrease with increasing initial concentration of fluoride. Adsorption amount of fluoride is highly dependent on solution pH. The presence of competitive ions in solution decreased the fluoride adsorption amount. Fluoride adsorbed can be effectively desorbed by NaOH solution and regenerated adsorbents still showed high adsorption capacity for aqueous fluoride. Results imply that La-ATP is an available substitute for the adsorptive removal of aqueous fluoride in water and wastewater treatment.

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