An Empirical Formula of Mean Specific Heat Capacity of Ideal Gases

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Abstract. The method of formulation of tabular data of mean specific heat capacity of gases is discussed and an empirical formula to fit these data is given in this paper. A linear function of temperature is chosen as the formula to piecewise fit mean isobaric specific heat capacity data over a wide range of temperature. For seven gases including air, CO, CO₂, O₂, N₂, H₂O and SO₂, the coefficients of the formula are regressed by means of least square method in the range of temperature 0° C to 1200° C and listed. The whole temperature interval is divided into 3 subintervals: $0 - 300^{\circ}$ C, $300 - 800^{\circ}$ C and $800 - 1200^{\circ}$ C, and fitting is done in the subintervals. The average deviations of the calculated values of the formula and reference values of mean isobaric specific heat capacity are less than 0.3% for all the gases in the temperature range from 0 to 1200° C, except CO₂. For CO₂, only in the subinterval of 300° C to 800° C is the average deviation 0.36%, and in other subintervals the average deviations are less than 0.3%.

Introduction

Calculation of enthalpy difference and thermodynamic energy difference is essential in the analysis and calculation of thermodynamic engineering. For ideal gases, enthalpy and thermodynamic energy are a function only of temperature, and then enthalpy difference and thermodynamic energy difference at two states are calculated as follows [1, 2]

$$\Delta h = \int_{1}^{2} c_{p} dT \,. \tag{1}$$

$$\Delta u = \int_{1}^{2} c_{\nu} dT \ . \tag{2}$$

Where h is enthalpy (kJ/kg), u is thermodynamic energy(kJ/kg), c_p is ideal gas isobaric specific heat capacity(kJ/kg $^{\circ}$ C), c_v is ideal gas isochoric specific heat capacity(kJ/kg $^{\circ}$ C), and T is temperature (K)

Although ideal gases do not exist in nature, the thermodynamic calculation based on ideal gases is basic for thermodynamic calculation for real gases. For gases at normal pressure or a little higher pressure, real gases can be treated as ideal gases. Eq.11 and Eq.12 are widely applied in thermal engineering for both ideal gases and real gases [3, 4, 5].

For ideal gases, specific heat capacity either at constant pressure or at constant volume is only a function of temperature. Equations of different forms [6, 7] are used to represent the relationship between specific heat capacity and temperature, with a polynomial being common. A cubic polynomial is often used to express the relation between gas specific heat and temperature

$$c_p = c_0 + c_1 T + c_2 T^2 + c_3 T^3 (3)$$

The coefficients of Eq. (3) are referred in many books [6, 7]. Therefore

$$\Delta h = \int_{1}^{2} c_{p} dT = c_{0} T_{2} + c_{1} T_{2}^{2} / 2 + c_{2} T_{2}^{3} / 3 + c_{3} T_{2}^{4} / 4 - c_{0} T_{1} - c_{1} T_{1}^{2} / 2 - c_{2} T_{1}^{3} / 3 - c_{3} T_{1}^{4} / 4 \quad . \tag{4}$$

If accurate calculation is not required, the value of specific heat capacities can be treated as a constant in the calculation of enthalpy difference and thermodynamic energy difference. If accurate calculation is necessary, the integration of Equation (1) and (2) is needed and the process of calculation, like Eq.(4), is relatively inconvenient. For convenience and accuracy, the concept of mean specific heat capacity [1, 7] is introduced in engineering analysis to simplify the calculation process. Note

$$\Delta h = \int_{t_1}^{t_2} c_p dt = \int_0^{t_2} c_p dt - \int_0^{t_1} c_p dt.$$
 (5)

$$\Delta u = \int_{t_1}^{t_2} c_{\nu} dt = \int_0^{t_2} c_{\nu} dt - \int_0^{t_1} c_{\nu} dt.$$
 (6)

Mean specific heat capacity at constant pressure and mean specific heat capacity at constant volume in the temperature range of $0 \sim t$ °C are defined respectively as

$$\left.c_{p}\right|_{0}^{t} = \frac{\int_{0}^{t} c_{p} dt}{t} \tag{7}$$

$$\left. c_{v} \right|_{0}^{t} = \frac{\int_{0}^{t} c_{v} dt}{t} \quad . \tag{8}$$

The enthalpy difference and thermodynamic energy difference can be written as

$$\Delta h = t_2 \cdot c_p \Big|_0^{t_2} - t_1 \cdot c_p \Big|_0^{t_1} \quad . \tag{9}$$

$$\Delta u = t_2 \cdot c_v \Big|_0^{t_2} - t_1 \cdot c_v \Big|_0^{t_1} \tag{10}$$

Thus the integral operation in Eq. (1) or Eq. (2) is converted to a simple arithmetic operation and the accuracy of integral calculation is still remained. This method has been widely employed in thermal engineering. Traditionally, based upon accurate data of specific heat capacity at different temperatures, values of mean specific heat capacity of gases are calculated on the interval from 0° C to arbitrary temperature t and listed in the tables for use [1, 8].

To keep the table spaces compact, the temperature interval in the table of mean specific heat capacity is wide. Interpolation calculation is usually required to determine the mean specific heat capacity on the region from 0 to temperature t ($^{\circ}$ C) and inconvenience is obvious. It is necessary and useful to correlate the tabular data of mean specific heat capacity with temperature to obtain a simple equation to further simplify the calculation for enthalpy difference in engineering applications.

Correlation of mean specific heat capacity data to temperature

The equation used for correlating the mean specific heat capacity data with temperature should be simple in form and has reasonable accuracy for calculation. Thus obtained equation is accordance with

that if we use a polynomial to fit all data in the whole range of 0-1200 °C, only a cubic or higher polynomial can give good accuracy of fitting. But a cubic polynomial is complex and not desired. Through examining the mean specific heat capacity data in literatures [1, 8] we divided the whole temperature range into several subintervals and on each subinterval chose a linear function of temperature, Eq. (11) to fit the data of mean specific heat capacity with least square method.

$$c_p \Big|_0^t = a + b \cdot t \tag{11}$$

A simple formula to correlate mean isobaric specific heat capacity with temperature is thus obtained. In this way the accuracy and simplicity of calculation of enthalpy difference can be kept. It is meaningless to adopt a more complex function to improve fitting accuracy. If the formula is complex in form, the direct integral calculation of Eq. (1) and Eq. (2) would be more proper.

For the data of mean specific heat capacity of seven common gases in the literature [1, 8], the regressed coefficients and deviations of Eq.(11) are shown in Table 1.

Table 1 Coefficients of Equation (11)

No.	gas	а	b	δ_{max} [%]	δ_{ave} [%]	Temperature
						[℃]
1	O_2	0.91320	1.1700×10 ⁻⁴	0.19	0.18	$0 \sim 300$
		0.91175	1.3257×10^{-4}	0.18	0.11	$300 \sim 800$
		0.94720	8.7000×10^{-5}	0.08	0.06	$800 \sim 1200$
2	N_2	1.0378	3.3000×10^{-5}	0.14	0.13	$0 \sim 300$
		1.0186	9.7143×10^{-5}	0.13	0.08	$300 \sim 800$
		1.0202	9.7000×10^{-5}	0.08	0.06	$800 \sim 1200$
3	СО	1.0386	4.6000×10^{-5}	0.18	0.15	$0 \sim 300$
		1.0194	1.1171×10^{-4}	0.11	0.06	$300 \sim 800$
		1.0296	1.0000×10^{-4}	0.06	0.05	$800 \sim 1200$
4	CO_2	0.8181	4.4600×10^{-4}	0.33	0.30	$0 \sim 300$
		0.8731	2.7143×10^{-4}	0.55	0.36	$300 \sim 800$
		0.9504	1.7000×10^{-4}	0.16	0.11	$800 \sim 1200$
	H_2O	1.8561	2.0100×10^{-4}	0.32	0.28	$0 \sim 300$
5		1.8234	3.1229×10^{-4}	0.19	0.12	$300 \sim 800$
		1.8044	3.3900×10^{-4}	0.06	0.04	$800 \sim 1200$
6	Air	1.0026	5.1000×10^{-5}	0.17	0.13	$0 \sim 300$
		0.9865	1.0571×10^{-4}	0.08	0.04	$300 \sim 800$
		0.9972	9.3000×10^{-5}	0.08	0.06	$800 \sim 1200$
7	SO_2	0.6081	2.6600×10^{-4}	0.13	0.10	$0 \sim 300$
		0.6460	1.5029×10^{-4}	0.42	0.28	$300 \sim 800$
•	· <u>2</u>	0.6992	8.2000×10^{-5}	0.28	0.22	$800 \sim 1200$

Note: $\delta_i = (\text{cal. value} - \text{ref. value.}) / \text{ref. value}, \ \delta_{max} = \max\{ \mid \delta_i \mid , i=1,2,...N \}, \delta_{ave} = \Sigma \mid \delta_i \mid / N$

As can be seen from Table 1, Eq.11 is satisfactory. The average deviations of the calculated values of Eq.11 and reference values of mean isobaric specific heat capacity are less than 0.3% for all the gases in the temperature range from 0 to 1200° C, except CO₂. For CO₂, only in the subinterval of 300 °C to 800 °C is the average deviation 0.36%. The maximum deviations are 0.55% for CO₂ in the range of 300 °C to 800 °C and 0.42% for SO₂ in the same range respectively. For other gases, the maximum deviations are all below 0.35% in the whole temperature range. Eq.11 could offer good enough accuracy to meet the requirements of engineering calculation. This indicates that the method

used to fit mean specific heat capacity data in this paper is correct and valid and therefore the formula obtained has high accuracy.

According to Mayer formula $c_p - c_v = R$ and the definitions of mean specific heat capacities at constant pressure and constant volume, the following formula is derived easily

$$c_{\nu}\big|_{0}^{t} = c_{p}\big|_{0}^{t} - R \tag{12}$$

Where R is gas constant (kJ/kg·K). From Eq. (12) and Table 1, the formula and its coefficients of mean isochoric specific heat capacity are therefore derived with ease.

Conclusion

The method of formulation of mean specific heat capacity data in tables was discussed in this paper. A linear equation of temperature was used to fit the data of mean specific heat capacity and an empirical formula calculating the mean specific heat capacity over the range of 0 - t (°C) was obtained. To improve the formula accuracy, fitting should be performed piecewise over a wide range of temperature. As instances, the data of mean isobaric specific heat capacity were fitted for 7 gases over the range of 0-1200°C and the coefficients of the formula regressed were regressed. Calculation and analysis indicate that the method used to fit mean specific heat capacity data in this paper is correct and valid, and the formula obtained is simple in form and accurate in calculation. The application of the formula of mean specific heat capacity proposed in this paper can simplify the process of calculation on the enthalpy difference and thermodynamic energy difference of gases.

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