

# Research and Application of Fluorine Complex Acid Plug Removal and Sand Consolidation Agent

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**Abstract.** Fluorine complex acid plug removal and sand consolidation agent is composed of trifluoroacetic acid, corrosion inhibitor, complexing agent, surface active agent. In this paper, the reaction mechanism, clay dissolution quantity, change of formation permeability, resistance to erosion intensity of fluorine complex acid plug removal and sand consolidation agent were studied, the experimental results showed that the fluorine complex acid plug removal and sand consolidation agent can not only relieve the mud pollution, but also firm sand when enhance the permeability. This new agent will be applied to the mud plugging and fine sand wells.

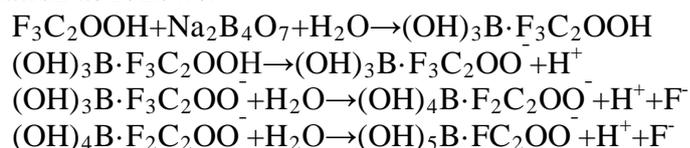
## Introduction

During the process of window sidetracked hole of low pressure heavy oil block of Liaohe Oilfield, a large amount of alkaline mud in near wellbore zone emulsify with heavy oil when the well completion production[1]. When open well production, thin oil wells shut down because of the mud and powder sand output or reservoir drainage difficulty caused by strata equilibrium conditions change in high clay content stratum[2]. These two blocks will cause stuck pump and frequent workover or shut.

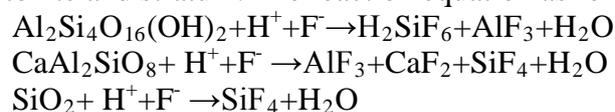
In view of the above situation, a fluorine complex acid plug removal and sand consolidation agent has been developed, and the mechanism, clay dissolution rate, permeability and core anti erosion ability also been studied. The agent can dissolve clay and generate vitreous nano coating which can mix the remaining clay and fine silt particles together as the shape of skeleton, so as to realize plug removal and sand consolidation integration.

## Plug removal and sand consolidation mechanism

Trifluoro acetic acid and borax reaction generated fluorine complex acid, which can slow hydrolysis generated complexing anions under formation conditions, and release  $H^+$ ,  $F^-$  which up to  $3H^+$ ,  $2F^-$ , this is a triple ionization of acids. It is suitable for oil deep processing because its dissolution capacity is stronger than mud acid, and also has slow response speed. The reaction equation as follows:



Hydrolysis of fluorine complex acid generate  $H^+$  and  $F^-$  which can dissolved components of bentonite and stratum. The reaction equation as follows:



Because the dissolution of bentonite, argillaceous and a small amount of silica sand, the formation permeability increases.  $(OH)_4B \cdot F_2C_2OO^-$  and  $(OH)_5B \cdot FC_2OO^-$  generated by the hydrolysis of complex can react with residual clay and compress the clay to be lamellar which can

adsorb on the surface of the sand. In addition they also can react with the surface of quartz and generate a coating of crystalloid fluorine boron[3]. The coating thickness is only in the nanometer range, and the porosity and permeability of the reservoir will not lower than before.

In summary, fluorine complex acid can dissolve clay, argillaceous and fine quartz effectively, and can improve the permeability and also can form sandstone skeleton which can coat residual clay and make it in the reservoir stability.

### The effect of bentonite

5 g of level II bentonite were immersed in the following two solution, Solution A contains 12% HCl and 3% HF, Solution B contains 10%  $(OH)_3B \cdot F_3C_2OOH$  solution. Reacting under the condition of 60 °C for 24 h, then washing with distilled water and drying. The result of analyzing with X-ray diffraction is shown in figure 1.

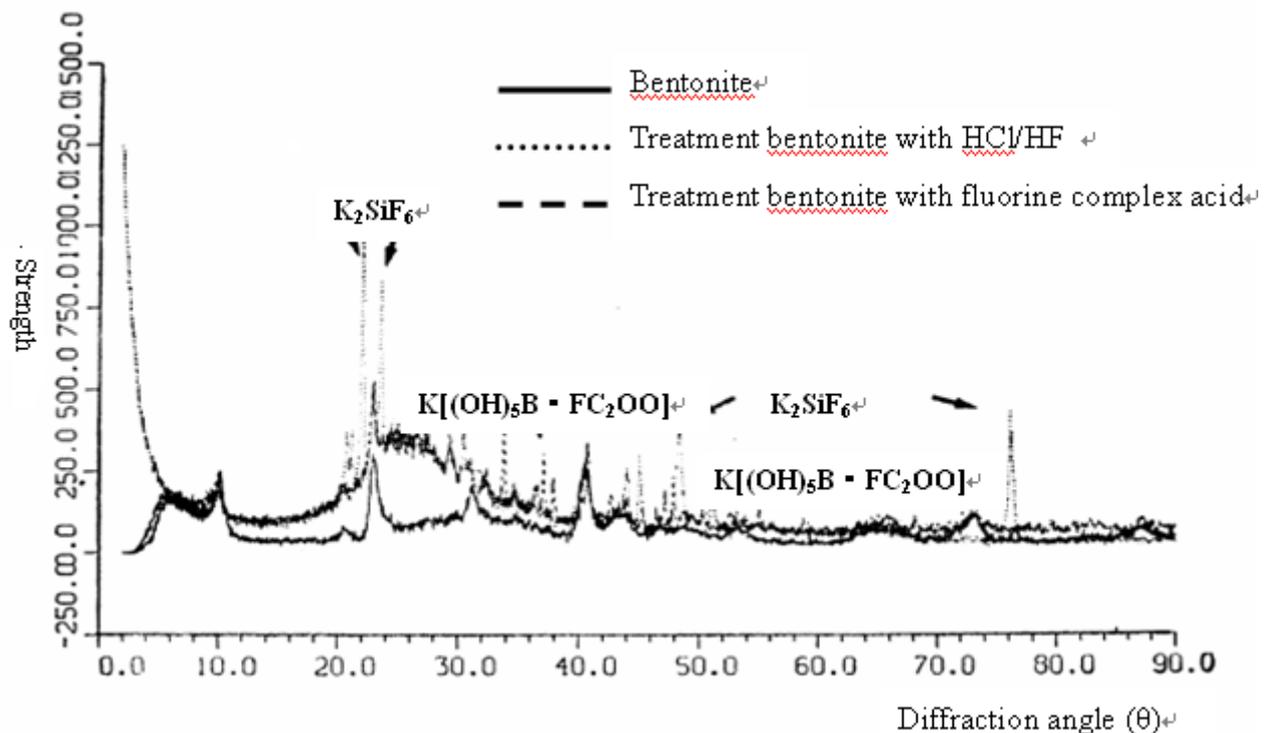


Fig.1. The result of analyzing with X-ray diffraction

Bentonite react with 12% HCl/3% HF to generate  $K_2SiF_6$  precipitate. The upheaval of the peak shows that the high content of the new compound.  $K_2SiF_6$  has large crystal size so it can not dissolve in water, this is a major factor of secondary pollution in treatment process of mud acid.

Bentonite react with 10%  $(OH)_3B \cdot F_3C_2OOH$  to generate  $K[(OH)_5B \cdot FC_2OO]$ . From the small peak can know the content of  $K[(OH)_5B \cdot FC_2OO]$  is small. Further with scanning electron microscope (SEM) know bentonite crystalline of  $K[(OH)_5B \cdot FC_2OO]$  is coated with nano coating[4]. So it not only won't produce secondary pollution, but also has very important effect on stability of clay and formation of the sandstone framework.

By quantitative determination can know that the bentonite dissolution ability of 10%  $(OH)_3B \cdot F_3C_2OOH$  is 1000mg/100mL which greater than 870mg/100ml of soil acid.

## Analysis of core treatment with fluorine complex acid

**Experiment of core selection.** By cold block 43 core group remove type I and II core, type II core than I core, potassium feldspar, original liquid phase permeabilities for  $80 \times 10^{-3} \text{ g m}^2$ . The analysis of core components in Table 1 by XRD.

Remove type I and II core from Leng 43 block core group. Type II core has higher content of potash feldspar than type I core. The original liquid phase permeabilities is  $80 \times 10^{-3} \mu\text{m}^2$ . The XDR analysis results of core components is shown in Table 1.

Tab.1. Petrophysical and chemical properties of two kinds of sandstone

Mineral (weight percentage)	Component	Type I sandstone	Type II sandstone
+		85-90	70-90
feldspar	Microcline	3-7	5-15
Maria glass	Muscovite	1	Tiny
	Chlorite	Tiny	—
Carbonate	Dolomite	2-5	Tiny
Clay	Kaolinite	1-3	—
	Glimmerton	—	5-10
	Glimmerton + Mixing layer clay	1-3	—
	Iron pyrite	Tiny	—
	Iron oxide and Hydroxide	—	1-2
Porosity(%)		21.7	17-18
Solubility(%)	15%hcl	7.5	4.3
	12%hcl/3%HF	22.5	31.2
Fe dissolved in HCl		0.07	1.0

**$\text{K}_2\text{SiF}_6$  generated test and observation after treated core with 12% HCl/3% HF.** Type II sandstone is selected for experiment for its higher potash feldspar content to be easy tested. Core specifications is  $8.0 \times 2.5 \text{ cm}$ , first washed with 15% hydrochloric acid about 10 times of the pore volume, until the core permeability reached stable. Then injected 12% HCl/3% HF acid of 10 to 15 times pore volume into the core with flow rate of 2ml/min, acid liquid residence time is 10 minutes, the test temperature is  $60^\circ\text{C}$ . Analyse Si, Al, K and F of effluent during the test, the result is shown in Figure 2.

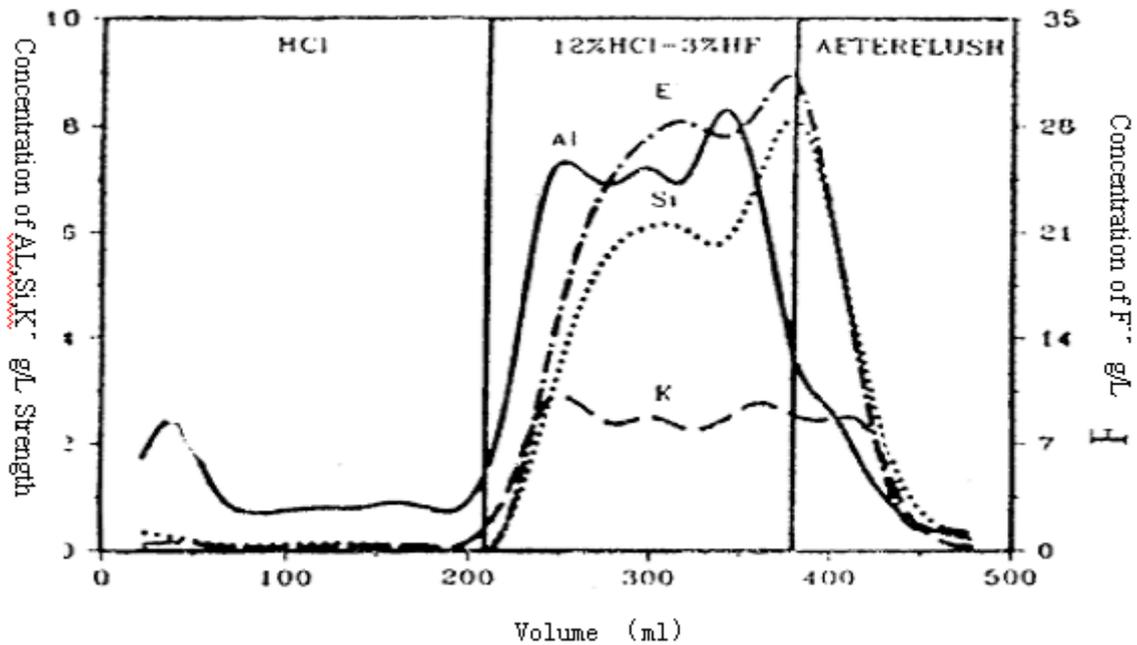


Fig.2. Effluent analysis of type II sandstone treated by 12% $\text{HCl}/3\%\text{HF}$

From the curve can know that content of Si is lower than Al, it means the consumption of Si, and change way of fluoride is similar to that of Si. The content of Si, Al, K in the outflow has the same tendency of the contents change in the whole flow test, and there is a suddenly-lowering when injection fluids is 350ml, this is owing to the saturation state of Si, Al, K and the secondary precipitate of  $\text{K}_2\text{SiF}_6$  in core. In addition, there are a large amount of sediment clogging pipes in the exit of core during the process of injection of 12% $\text{HCl}/3\%\text{HF}$  acid. X-ray diffraction analysis confirmed that sediment is  $\text{K}_2\text{SiF}_6$ , this is because the outlet pipe temperature is lower than the temperature of the core. From Figure 2 can know that the content of Si, Al, K has a suddenly-lowering when cleaning fluid is between 400 to 500ml.

**$\text{K}[(\text{OH})_5\text{B}\cdot\text{F}_3\text{C}_2\text{OO}]$  micro crystal growth test and observation after treated core with  $\text{OH}_3\text{B}\cdot\text{F}_3\text{C}_2\text{OOH}$ .** Also take Type II sandstone for experiment. Core specifications is 8.0x2.5cm, first washed with 15% hydrochloric acid about 10 times of the pore volume, until the core permeability reached stable. Then injected 10% $(\text{OH})_3\text{B}\cdot\text{F}_3\text{C}_2\text{OOH}$  acid of 10 to 15 times pore volume into the core with flow rate of 2ml/min, acid liquid residence time is 10 minutes, the test temperature is 60°C. Analyse Si, Al, K and F of effluent and  $(\text{OH})_5\text{B}\cdot\text{F}_3\text{C}_2\text{OO}$  during the test, the result is shown in Figure 3.

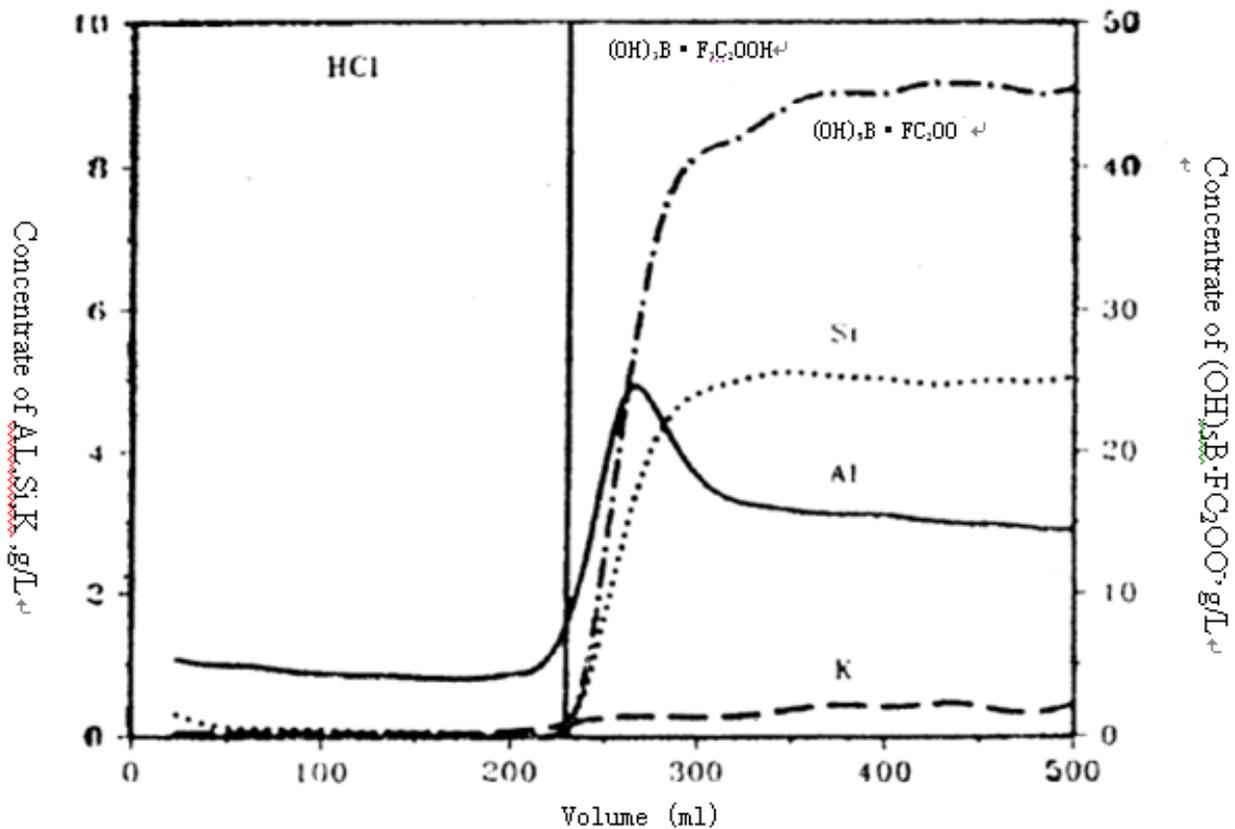


Fig.3. Effluent analysis of type II sandstone treated by 10% $(OH)_3B \cdot F_3C_2OOH$

After pumping  $(OH)_3B \cdot F_3C_2OOH$  acid into the core, there is only a very small amount of crystal in the outlet of core. From X-ray diffraction analysis can know the crystal is  $K[(OH)_5B \cdot FC_2OO]$ . Content of Si higher than the content of Al in the effluent curves, and the content curves of Si,  $[(OH)_5B \cdot FC_2OO]^-$ 、 $K^+$  is very flat, that means there is only a very small amount of  $K[(OH)_5B \cdot FC_2OO]$  formed, so it will not cause the decrease of core permeability.

**By 10%  $(OH)_3B \cdot F_3C_2OOH$  before and after comparison of permeability of acid and acid treatment of core 12%HCl/3%HF.** Take six blocks of Type II and Type I sandstone for experiment. Core specifications is 8.0 x 2.5cm, first washed with 15% hydrochloric acid about 10 times of the pore volume, and then pump into about 20 times of pore volume treatment fluid, the test temperature is 60°C. Stop injection for 10min before the end of acid injection and determination of the ultimate permeability. The result is shown in Table 2.

Tab.2. core flow experimental data

Sandstone	Acid	Salt water permeability before treatment ( $\times 10^{-3} \mu m^2$ )	Salt water permeability after treatment ( $\times 10^{-3} \mu m^2$ )
II	12%HCl/3%HF	80	115
II	10% $(OH)_3B \cdot F_3C_2OOH$	80	105
I	12%HCl/3%HF	220	1
II	10% $(OH)_3B \cdot F_3C_2OOH$	110	210
II	12%HCl/3%HF	15	3
II	10% $(OH)_3B \cdot F_3C_2OOH$	2	5.5

The serious blocking in outlet tube of core slot. See from the table that only one core permeability is increased after treatment of 12%HCl/3%HF, but outlet tube of core slot is seriously blocked. The permeability is increased greatly after treatment of 10% $(OH)_3B \cdot F_3C_2OOH$ , that means the effect of  $(OH)_3B \cdot F_3C_2OOH$  to remove formation plugging is very good, and permeability

ratio is greater than 1.

**salt water flushing ability of artificial cores after acid treatment of 10% $(\text{OH})_3\text{B}\cdot\text{F}_3\text{C}_2\text{OOH}$ .** Select 16-24 mesh rock particles from type I and II core respectively, mixed with 10% bentonite, and put it 100ml into measurer of 2.5cm and compact in 0.1MPa, soaking for 48 hours with  $(\text{OH})_3\text{B}\cdot\text{F}_3\text{C}_2\text{OOH}$ , then inject 12000ml 5%KCl of 400PV with flow rate of 10ml/min. It does not appear collapsing and breaking of rock particles in the scour process, that means  $(\text{OH})_3\text{B}\cdot\text{F}_3\text{C}_2\text{OOH}$  has good effect on stability of clay and sand consolidation.

### **Field application and effect analysis**

From January 21,1999 the field application started, 14 wells had been operated until November 30,2000. A good results can be known from the successful rate of construction and increase oil index.

1613 wells of Xinglongtai oil production plant was shutoff for generate of mud and fine sand in January 21,1999. The reservoir thickness is 21m, layer number is 7, oil temperature is 51 °C. Used 15 tons of the agent for unplugging on January 21, and opened the wells on January 25. The daily output of liquid reached 13m<sup>3</sup>,and daily output of oil reached 12 tons. The daily output of oil is to maintain at 3 tons after continuous production for 22 days.

3023 wells of Shuguang oil production plant was shutoff for generate of mud and fine sand in December,1999. The reservoir thickness is 17m, layer number is 5, oil temperature is 50 °C. Used 15 tons of the agent for unplugging on December 25, and opened the wells on December 31. The daily average output of oil is 3 tons in January, and 5 tons in February, and 4.6 tons in March. The cumulative oil production is 343t by the end of May 31.

### **Conclusion**

Fluorine complex acid plug removal and sand consolidation agent is triple ionization of acids, and it can used for deep treatment of oil layer. 14 wells which has clay content between 10% to 30% were constructed, the effective rate was 85%.

Dissolve ability of clay of fluorine complex acid plug removal and sand consolidation agent is 1000mg/100ml,so it can remove the mud plugging.

The agent can react with quartz sand, then generate a coating of crystalloid fluorine boron and form sandstone skeleton which has capability of resistance to scour upto 400PV.

Permeability ratio of fine powder sand Wells is greater than 1 after unplugging with fluorine complex acid plug removal and sand consolidation agent.

The cumulative incremental oil of this 14 wells is 3864.7 tons, input-output ratio reached 1:2.8, and achieved good economic and social benefits.

### **References**

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