

Design and numerical simulation of an immunoisolation perfusion co-culture bioreactor for expansion of NSCs

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Abstract. Considering the immunoisolation from the neural stem cells (NSCs) and endothelial progenitor cells (EPCs), the requirements of the carrier, shear tolerance and other factors, this study designed an immunoisolation perfusion co-culture bioreactor system, by dynamic perfusion culture environment of its upper and lower bi-levels and the immunoisolation of intermediate polycarbonate membrane, combining the measure of embedding NSCs and EPCs with calcium alginate/gelatin microbeads, integrating hypoxic environment effectively to achieve the expansion of NSCs. The results show that the microbeads are more evenly distributed under dynamic perfusion conditions, the velocity of medium is slightly larger near polycarbonate membrane and the culture chamber wall surface, and has more balanced distribution of other regions, static pressure and dynamic pressure of the culture chamber are generally evenly distributed. Studies showed that the expansion of NSCs under perfusion conditions, is able to meet the mass transfer and provide a stable environment to the neural stem cell expansion.

Introduction

Neural stem cells (NSCs) have self-renewal, replication capacity and multi-differentiation potential. They can differentiate into neurons, astrocytes and oligodendrocytes, which can be applied to the treatment of Parkinson's disease, spinal cord injury, cerebrovascular disease, etc [1-3]. At present, the application and research of NSCs include direct use of cell transplantation for replacement therapy, using NSCs as gene carrier and carrying the target gene with therapeutic action and self-repair of NSCs induced to self-differentiation, etc [4-6]. At the same time, with the continuous further research of the human nervous system and the rapid development of clinical cell therapy, the quantity and quality of NSCs have been put forward higher requirements. Therefore, how to harvest a sufficient number of NSCs on the basis of effectively maintaining the stemness, is the key issue to be resolved.

The main methods of *in vitro* culture of NSCs were the cultivation of the sphere in the culture vessel by suspension method and the culture on the surface of the treated culture environment in a single wall [7,8]. The culture way of NSC sphere is simple to operate, in which cell number is relatively large. NSC spheres can be blown about and differentiate into specific cells through different induced growth factors. But the shortcoming is, with the increase of the sphere size, the requirement of mass transfer cannot be satisfied. So the dark core was formed inside the sphere, where apoptotic, necrotic, and phagocytic cells were easily appeared, and perhaps even the hollow

of the NSC spheres [9]. Monolayer adhesion method can effectively meet the requirements of material transfer. However, the cell adhesion area is small in this way, which limits the increment of cells, and is therefore not conducive to the cell expansion. Simultaneously, if the cells are directly exposed to the dynamic liquid environment, the shear stress will cause damage to NSCs, resulting in decreased activity, and even cell death [10].

The NSCs were cultured in a suitable bioreactor system with an ideal three-dimensional (3D) cell carrier, which can satisfactorily solve the problem above mentioned. The ideal 3D cell carrier can provide attachment sites for NSCs, and allow timely diffusion of nutrients and metabolites. It is easy to set up connections between cells, can make NSCs a suitable spatial distribution and cell connections, and also provide specific growth and differentiation signals for cells. In addition, the cell carrier can prevent NSCs from being more sensitive to the shear force in dynamic environment, which has a very good protection effect. The suitable dynamic bioreactor system can not only provide enough residence time for the internal culture of NSCs, effectively meet the requirements of material delivery, but also achieve the effective isolation of stromal cells in co-culture system [11,12].

Endothelial progenitor cells (EPCs) have the function of mobilization, proliferation, migration and homing to sites of injury and differentiation to vascular endothelial cells in the effect of specific factors, which make it available to be used for co-culture with NSCs. Research shows that [13,14], neurogenesis occurs commonly after the angiogenesis. Neurogenesis after injury phenomenon is also appearing along the vessel path with a large number of vascular endothelial differentiation. Angiogenesis provides a good platform for neurogenesis. And EPCs also showed a significant neuroprotective effect. Therefore, neural microenvironment formed by co-culture of EPCs and NSCs can promote the proliferation of NSCs to a large extent; In addition, EPCs can delay the differentiation of NSCs by secreting cytokines such as VEGF and FGF-b, etc [14]. Therefore, if the co-culture was carried out using EPCs and NSCs, it is expected to achieve large scale expansion of NSCs on the basis of effectively maintaining NSCs dryness.

Based on this, we designed an immunoisolation perfusion co-culture bioreactor (IPCB), which is used by two kinds of different cells in the dynamic perfusion environment with up and down bi-level culture chamber, and the numerical simulation and flow field analysis of IPCB were also carried out.

Software and methods

Gambit and Fluent

ANSYS Fluent software (ANSYS, Canonsburg, PA, USA) can be used to realize the mass transfer in a bioreactor culture system. It provides ideal grid adaptability and can solve complex fluid problems easily by an irregular grid, which is provided by complex geometry. In view of the characteristics of every physical problem in fluid dynamics, a suitable numerical solution is provided by ANSYS Fluent in order to achieve optimality in multiple aspects such as computation speed, stability, and precision.

On the basis of computational fluid mechanics principle, with the help of fluent software, the mass transfer analysis in an IPCB provides important theoretical and reference data for the subsequent cell and tissue experiments, to make it more effective application in the 3D fabrication of tissue engineered cartilages/bones.

Physical and simplified model of bioreactor flow

To simplify the calculation, the flow of the static environment was treated as a two-dimensional problem. As the rotation speed of the IPCB used in further fabrication experiment was quite low, the calculated speed of the IPCB was therefore set at 50 rpm, and the flow field in IPCB with this rotating speed still remained laminar flow. Therefore, laminar modeling of Fluent could be used for numerical simulation calculations.

Based on this, mass fraction distribution of microspheres constructs in an IPCB during the culture process was calculated. The specific conditions and calculation objects were as follows: in order to calculate the force condition and its distribution around the flow field of the microspheres

constructs, the three-dimensional section size of the constructs was set to a cane with a middle straight height of 5 mm, dimension of 70 mm and cane angle of 60°. Changes in the simulation calculations, collected from different section, were analyzed when the rotation direction and speed of the IPCB was determined. The partition of the 3D mesh and constraints that defined the physical boundaries above were shown in Table.1&2

Table 1 Parameters of bioreactor		Table 2 Parameters and boundary conditions	
Dimension (mm)	70	Culture medium density (kg/m ³)	1050
Height (mm)	5	Dynamic viscosity (Pa.s)	3×10 ⁻³
Cone angle (°)	60	Vessel rotational velocity (rpm)	50
Dimension of entrance (mm)	5	Fluent version	3d
Dimension of outlet (mm)	5	Solver	Segregated, implicit
		Pressure	Body-force weighted
		Pressure-velocity coupling	PISO
		Momentum	Second order upwind
		Flow	laminar

Experiment Purpose

Considering the immune isolation, carrier requirements, shear tolerance and other factors of MSCs and EPCs, the project designed immunoisolated perfused co-culture bioreactor (IPCB, shown in Fig.1) for two types of different cells. The dynamic perfusion environment provided by the upper and lower bi-level of the culture chambers and immune isolation of intermediate polycarbonate diaphragm, combined with calcium alginate/gelatin microbead encapsulated NSCs and EPCs and other measures, can effectively integrate hypoxic environment to achieve NSCs efficient amplification purposes. The project will design and prepare polycarbonate diaphragm which have immune isolation and investigate diaphragm's flow field distribution, shear and dynamic pressure changes and mass transfer efficiency on both sides culture chamber by both simulation and experiment aspect.

Results and Discussion

Design and structure of IPCB

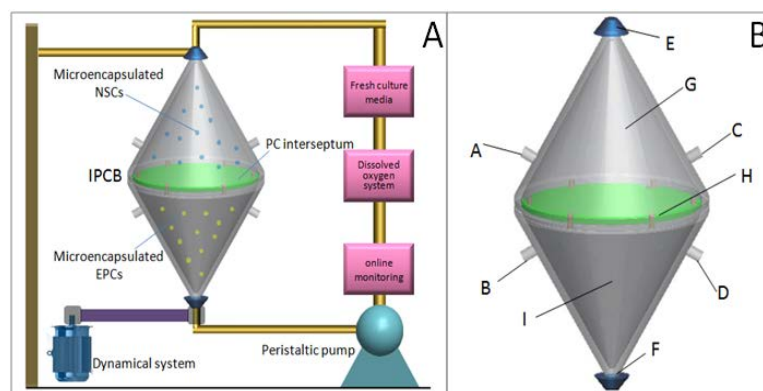


Fig.1 Schematic for structure and function of immunoisolation perfusion co-culture bioreactor system and cell culture chamber. (A) Immunoisolation perfusion co-culture bioreactor system; (B) Cell culture chamber with up and down bi-level design.

In the IPCB, as shown in Fig.1B, A-D are sampling ports, E is the medium outlet of perfusion circuit, F is the medium entrance of perfusion circuit, G is the upper culture chamber, which will be used for culture of calcium alginate/gelatin microbeads embedded with NSCs; I is the lower culture chamber, which will be used for culture of calcium alginate/gelatin microbeads embedded with EPCs; Between two layers of polycarbonate diaphragm is H, which can be used for immune isolation of dynamic co-cultured NSCs and EPCs.

Flow field simulation of IPCB

In Fig.2, A is model grid distribution of three-dimensional dynamic reactor system of IPCB.

Distribution of microbeads in X-axis direction of the upper and lower bi-level culture chambers is shown in Fig.2B, in the dynamic culture process (50rpm speed, rotate along the Z axis), we can see that most of NSCs embedded in the micro plastic beads of upper culture chamber are in the middle of the polycarbonate diaphragm, a precious few of them located at the top, however, distribution of micro plastic beads in the down culture chamber are more scattered. C is the dynamic pressure distribution in the left side of cultivation chamber.

As can be seen from Fig.2D, the hydrostatic pressure distribution of IPCB's upper and lower levels in culture chambers is more evenly distributed; as medium speed in culture chamber, the speed of the regions near polycarbonate diaphragm and the upper and lower layers of the culture chamber wall surface are slightly higher, other regions are more balanced distributed.

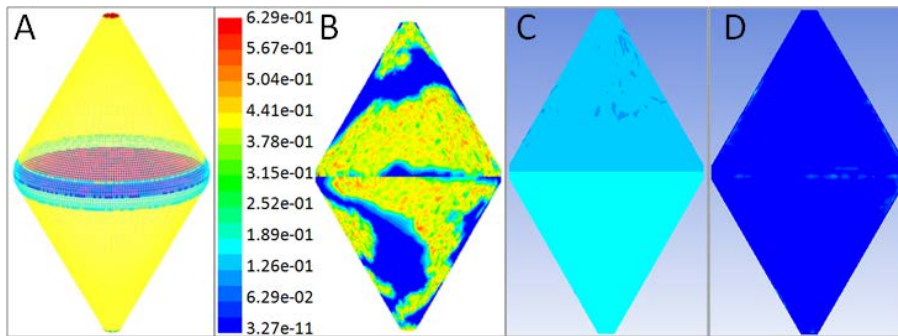


Fig.2 Simulation mesh distribution of flow field in IPCB and flow field analysis of up and down bi-level culture chamber.

IPCB culture chamber flow field analysis

Fig.3 is a sectional distribution of up and down layer, $\pm 10\text{mm}$, $\pm 20\text{mm}$, $\pm 30\text{mm}$ and $\pm 40\text{mm}$ based on polycarbonate membrane. Dynamic pressure distribution of cell plastic beads surface in IPCB culture chamber of upper and lower levels (A). Dynamic pressure distribution(C) and velocity distribution(D) of medium. Viewing the flow field analysis from the section of upper and lower levels(Fig.3A), plastic beads in the cell wall surface have the higher dynamic pressure value and have lower value in the central region; The results of cell distribution are showed on Fig.3B, plastic beads NSCs are mostly distributed near the polycarbonate membrane in the middle, a small part is at the top; And plastic beads are more scattered distribution in the lower level. Known from the dynamic analysis (Fig.3C), the position of polycarbonate membrane in the middle has the minimum value of the dynamic pressure, the remaining parts have the greater value because of the perfusion medium can eliminate the difference between the gravity of micro plastic beads and the buoyancy of medium. And the velocity of the edges, the top and the bottom have the greater value(Fig.3D), because the velocity distribution is the same as Fig.3C.

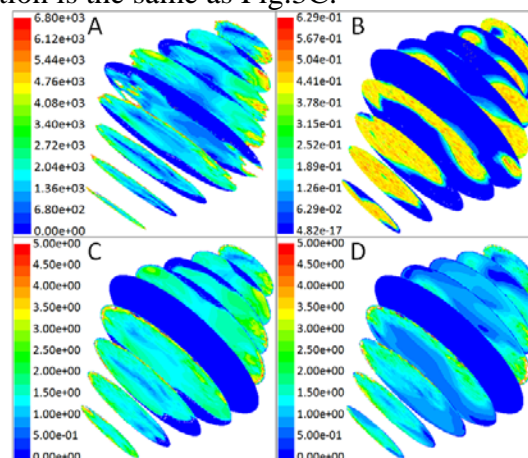


Fig.3 low field analysis of up and down bi-level culture chamber of IPCB. Sectional distribution of up and down layer, $\pm 10\text{mm}$, $\pm 20\text{mm}$, $\pm 30\text{mm}$ and $\pm 40\text{mm}$ based on polycarbonate membrane. Dynamic pressure distribution (A) of surface on microbeads cultured in bi-level, the distribution of the cultured NSCs and EPCs (B), dynamic pressure distribution of the medium (C) and the velocity distribution (D) of up and down bi-level.

Conclusion

In summary, the micro plastic beads are more evenly distributed under perfusion conditions, in favor of the mass transfer. The velocity of medium is slightly larger near polycarbonate membrane and the culture chamber wall surface, and has more balanced distribution of other regions, thus greatly reducing the shear. Static pressure and dynamic pressure of the culture chamber are generally evenly distributed, providing a stable environment to the neural stem cell proliferation.

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