

Solid-liquid flow model and the impact of turbulent flow field on stirred parameters for oil chili sauce

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ABSTRACT: From the study of mixed solid-liquid flow characteristics of viscous liquid, solid-liquid model of two phase flow for oil chili sauce in the stirring apparatus is presented in this paper. The impacts of turbulent flow field for stirred parameters in the stirring apparatus are studied. Combining with the study of oil chili fluid flow characteristics, proposes the solid flow model and turbulent flow field on stirre parameters on oili sauce, for determining of the stirring speed and so on.

KEYWORD: Oil chili sauce, Solid-liquid flow model, Stirring device, Turbulence model

1 INTRODUCTION

Guizhou condiment is the main of chili. And there are 120 chili varieties in the Guizhou province. It is difficult to store fresh chilli, and dry chili is low add-value. Therefore, deep processing of chili in creating added value is very important. Oil chili sauce which contains chili, lobster sauce, edible oil, Chinese prickly ash and meat is a high value-added deep-processing of chili. For traditional automatic filling technology, solid-liquid ratio and filling accuracy already can't good meet mixed solid-liquid of oil chili sauce automatic filling requirement.

Mixed proportion and two-phase flow characteristics are the key technology to research the complex solid-liquid mixture filling for oil chili sauce. Further, the research of two-phase flow characteristics in solid-liquid mixing technology is important for filling machine development, and most researchers now focus on mixed characteristics, power consumption and flow characteristics. Liang super (Li Liang chao, 2014) Euler-Euler two-fluid model based on particle dynamics of sinking particles and floating particles of solid-liquid suspension characteristics were studied. Lucy Liu (Liu Yu ling, 2014) on the flow field in a stirred tank was analyzed. R. Angst, M. Kraume (R. Angst, 2006) in a stirred tank with three different power consumption of solid-liquid two-phase mixture was stirred at different concentrations were experimentally study also shows the results of experiments using CFD predictions need to be amended. This paper by drawing on the physical characteristics can be controlled stirring of other pharmaceutical and chemical properties of the reference material, and combined with the physical characteristics of the system itself chili oil, to carry out the relevant theoretical

and experimental studies, which made chili oil to ensure optimization of product quality and process stability parameters for the promotion of comprehensive utilization and deep development of pepper is of great importance.

2 CHILI LIQUID TURBULENT MIXING PLANT OIL SYSTEM MODEL

2.1 Basic features mixing process

According to the views of fluid mechanics, fluid can be divided into two major categories of ideal fluid and the actual fluid. Ideal fluid in the flow without resistance, is called a non-viscous fluid; When the actual fluid flow resistance within the friction (or shear), called a viscous fluid. According to the effect on the fluid shear stress and the shear rate, the relationship between the viscous fluid and can be divided into Newtonian fluids and non-Newtonian fluid. After Newton fluid refers to the mechanical deformation extremely easily, and the shear stress and deformation rate is proportional to the low viscous fluid. All different from the Newtonian fluid are referred to as non-Newtonian fluid. Mixing oil system of chili liquid in the tank is a kind of solid-liquid mixed viscous liquid, obviously is a Newtonian fluid. Stirring can make two or more different material dispersed to each other, so as to achieve uniform mixing, also can accelerate the heat transfer and mass transfer process.

2.2 Mixing oil groove system chili liquid turbulence model

Mixing device in the main flow characteristic of fluid is turbulent, In theory, all turbulence can be full Navier-Stokes equations are solved numerically solving [4], conservation in the form of unsteady three-dimensional Renault (Reynolds) average Navier-Stokes equations as follows:

Continuous equation:

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i}(\rho u_i) = 0 \quad (1)$$

The momentum equation:

$$\frac{\partial \rho}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_j}(\rho u_i u_j) = -\frac{\partial P}{\partial x_i} + \frac{\partial \tau_{ij}}{\partial x_j} \quad (2)$$

Energy equation:

$$\frac{\partial}{\partial t}(\rho E) + \frac{\partial}{\partial x_j}(\rho u_j H) = \frac{\partial P}{\partial t} + \frac{\partial}{\partial x_j}(u_i \tau_{ij} + \lambda \frac{\partial T}{\partial x_j}) \quad (3)$$

In the formula,

$$\tau_{ij} = \mu_t \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} - \frac{2}{3} \delta_{ij} \frac{\partial u_k}{\partial x_k} \right)$$

Among them, ρ , t , u_i , x_j , P , E , H , T respectively, the density, time, velocity components, coordinate geometry, pressure and internal energy, enthalpy and temperature, turbulence viscosity coefficient, respectively, for the turbulent Prandtl constant, Reynolds stress, according to the influence of turbulence.

(1) the turbulence intensity

If mixing between shaft and blade groove for clearance, clearance area full of turbulent boundary layer can be thought of, during which time averaged velocity field distribution as follows:

$$\begin{cases} \bar{u}_\theta = \frac{u_2}{2 \arctg\left(\frac{\sqrt{R_e} \kappa}{2}\right)} \arctg\left(\frac{\sqrt{R_e} \kappa (r_1 - r_2)}{\delta}\right) & (r_1 \leq r \leq r_1 + \delta/2) \\ \bar{u}_\theta = u_2 + \frac{-u_2}{2 \arctg\left(\frac{\sqrt{R_e} \kappa}{2}\right)} \arctg\left(\frac{\sqrt{R_e} \kappa (r_1 + \delta - r)}{\delta}\right) & (r_1 + \delta/2 \leq r \leq r_1 + \delta) \end{cases} \quad (4)$$

The shear stress field is:

$$\begin{cases} \tau_{r\theta} = \frac{u_2 \sqrt{R_e} \kappa}{2 \delta \arctg\left(\frac{\sqrt{R_e} \kappa}{2}\right)} & (r_1 \leq r \leq r_1 + \delta/2) \\ \tau_{r\theta} = \frac{\mu u_2 \sqrt{R_e} \kappa}{2 \delta \arctg\left(\frac{\sqrt{R_e} \kappa}{2}\right)} & (r_1 + \delta/2 \leq r \leq r_1 + \delta) \end{cases} \quad (5)$$

Type, R_e as the Reynolds number; μ Is the drop-let deformation stress coefficient, equal to the ratio of shear stress and shear rate; κ for turbulent Karman constant, desirable $\kappa=0.2\sim0.4$, or use to calculate $\kappa=0.125R_e^{0.07}$; u_2 for the blade linear velocity; r_1 and r_2 the radius of the rotor and blade respectively.

(2) The Reynolds number

With chili oil system mixing Reynolds number increases, groove groove of the circulation flow pattern also were characterized by laminar flow, transition

flow and turbulence, < 50 , groove fluid performance for laminar flow; $50 < < 104$, groove fluid performance for transition flow; > 104 , groove fluid is turbulent.

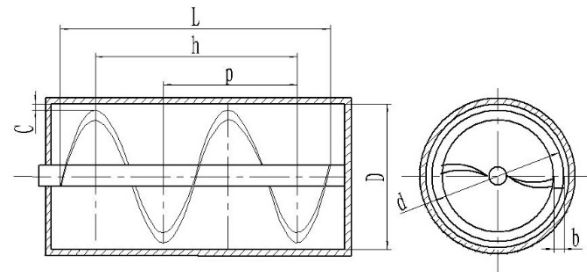
3 CHILI OIL SYSTEM FLUID FORM IMPACT ON MIXING PARAMETERS

Stirring device need to consider about stirring the material properties, mixing purpose, production requirements, production requirements, demand for power and equipment costs and so on.

3.1 The mixing mode and shape of the device

Stirring device can be divided into straight blade paddle, open turbine type, push, disk turbine, anchor, ribbon, spiral and other shapes, depending on the viscosity of different liquids can be divided into a low viscosity fluid mixing device, high viscosity liquid stirring devices.

It is difficult to achieve goals to adopt vertical mixing form because the filling equipment mixing oil groove of chili liquid viscosity is bigger and continuous stirring flow patterns and export more uniform flow material etc.so this paper used impeller type which is Horizontal spiral ribbon, horizontal mixing machine is comprised of a U-shaped trough, ribbon agitator blades and transmission components, as illustrated in Fig. 1.



C - blade and tank wall distance; D - agitation tank diameter; B - ribbon width; D - ribbon diameter; H - ribbon section height; P - pitch; L mixing plant total height
Fig. 1. Horizontal spiral ribbon agitator

3.2 Stirring device geometry parameter

(1) The diameter of the stirring shaft d_0

Generally should be calculated on torsional deformation, stirring shaft by combination of the torsion and bending moment, torsional deformation will cause the vibration of the state, make oil seal failure, so the shaft on the unit length should be the biggest torsion Angle limit within the scope of the permit,

$$d_0 \geq 155.4 \left(\frac{M_{nmax}}{[\gamma] G (1 - N_0^4)} \right)^{\frac{1}{4}} \quad (6)$$

The type, $[\gamma]$ it is permissible torsion Angle;
 M_{nmax} is the maximum torque shaft transmission, if
the drive for efficiency η , then $M_{nmax} = 9553 \frac{P}{n_d} \eta$; G
is the shaft material shear modulus of elasticity; N_0
the ratio of inner and outer diameters is hollow shaft.

(2) The mixing device blade diameter (screw
with diameter) d

According to the experiment, the slot size D
=100-600mm, tub a certain diameter, determines the
size of the impeller blade diameter and distance on
the surface of the cylinder body wall, namely clear-
ance, generally take $d/D=0.73-0.98$, according to
the characteristics of the slurry an material, through
mixing plant blade diameter to tank diameter is ob-
tained by mixing blade diameter.

(3) Pitch p

Experiment take: $p/d=0.386-2.15$. The radial
movement of fluid in the $p/d < 0.664$ there is no ob-
vious regularity, when p/d increases to 1.0, the
sharp rise in the radial velocity.

(4) The ribbon width

Experiment take: $b/d = 0.0836$ to 0.266 .

(5) The ratio of the wheel and shaft

Round the ratio of impeller diameter and the diam-
eter of shaft called round than, tell from the hydraulic
performance, reduce the ratio of the wheel and shaft,
can reduce the hydraulic friction loss, increase the
mixing push flow area, and is helpful for the improve-
ment of the cavitations resistance.

3.3 The Power of Stirred Device

The consumed energy of stirred device is mainly pro-
vided to the material in mixing plant to shear and cir-
culation. The mixing power means the energy that is
used to put the material into the slurry pool per unit
time, during mixing, but the energy that is consumed
in the shaft seal and transmission device is excludes.
There are 2 aims in calculating the stirring power.
One is to design or nuclear the stirred device and the
strength and stiffness of the stirring shaft. The other
is to select the gearing, such as the motor and trans-
mission. When some stirred device stir a certain phys-
ical properties of materials in a specific speed, the
power that stirred device work on the material is hap-
pening.

4 CRITICAL SPEED

The lowest stirring speed that can make solid-liquid
two phase flow achieve full state of suspension from
the bottom is called critical speed of revolution, N_{ja} ,
There were a number of critical speed, N_{ja} , of corre-
lations reference about solid-liquid two phase flow.
Referencing (Yang Feng ling, 2012) connection type
that belongs to Zwietering, blade mixing critical
speed can be written as:

$$N_{ja} = K d^{0.85} v^{0.1} d_p^{0.2} \left| g \frac{\rho_p - \rho}{\rho} \right|^{0.45} \left| 100 \times \frac{\rho_p \phi_v}{\rho(1 - \phi_v)} \right| \quad (7)$$

N_{ja} is the critical speed; K is the equation constant;
 v is kinematic viscosity of liquid; ρ is the density of
the fluid; ρ_p is the density of solid particles; d_p is the
diameter of the solid; ϕ is the solid volume fraction;
 d is the blade diameter; g is the acceleration of grav-
ity.

5 THE EXPERIMENTAL ANALYSIS AND CONCLUSION

According to the above theory, the main parameters
could be shown in table 1

Table 1 Main parameters of model (unit mm):

Number	parameters	data
1	Agitation tanks bore D	360
2	Ribbon diameter d	320
3	The distance between ribbon and wall C	20
4	Ribbon width b	40
5	Ribbon height h	800
6	Pitch p	800
7	Stirrer height L	800

(1)The calculation of power energy in stirring
test does not include the energy consumption in shaft
seal and transmission device, equipment debugging
test show that the consumed power of shaft seal is
bigger, is just the 5% to 10% of stirring the consumed
power. So when choose the stirring, motor the param-
eters should be reserved.

(2)In order to achieve the mixing uniform state
when stir chili liquid, the stirring of chili liquid is
firstly requested to provide certain amount of circula-
tion, to avoid dead zones in the stirring tank, and
make the spiral ribbon exceeds a certain speed(critical
speed), so that chili liquid is stirred achieve rapid con-
vective circular motion; and request the turbulence in-
tensity and shear velocity in the stirred tank is rela-
tively large, the shearing benefit to the dispersion of
chili dough in the tank and the strengthening of tur-
bulence expansion. Although higher speed may im-
prove the uniformity of chili liquid in the tank on the
overall, it has little effect on improving the filling uni-
formity, even affect the quality of filling oil chili.

(3)The width of helical ribbon have a great influ-
ence on the mixing efficiency, when the width of hel-
ical ribbon is doubled (from $b = 20$ mm to 40 mm),
chili liquid mixing efficiency nearly double and in-
creased significantly.

(4)The Change of screw pitch have little effect on
the rate of mixing, when the clearance of helical rib-
bon and tank wall is doubled within recommended
value, the mixed time increased less than 10%.

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