

Teaching Process Control Using The CSTH Model

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Abstract—This paper discusses a case-based approach to teaching process control involving modeling, measuring, PID and cascade control methods. In the traditional process control teaching, there are some problems such as knowledge points are taught without any example or taught by different examples, which make student be passive to study, and it's difficult to setup the whole knowledge system. Case teaching is an efficient method to help students understand the principles of process control and get the ability to solve practical problem. CSTH model is presented for the case which involves several knowledge points of process control in this article.

Keywords- *process control; continuous stirred tank heater; case teaching*

I. INTRODUCTION

Process control has become increasingly important in the process industries as a consequence of global competition, rapidly changing economic conditions, and more stringent environment and safety regulations. Process control is also a critical concern in the development of more flexible and more complex processes for manufacturing high value-added products[1]. As one of the compulsory and specific courses in the major of automation, process control involves theoretical knowledge and mathematical background and even engineering models. A good control engineering course should be accompanied by hands-on experiments[2]. This teaching method is called case teaching. It's obvious that how difficult it is to learn the concepts involved in process control without real models. Case teaching has a long history in business, law, and medical education. In recent years, case study has also been used for science and engineering education. Cases can be used not only to teach scientific concepts and content, but also process skills and creative thinking, because many perfect cases are based on contemporary, and contentious engineering problems. Therefore, choosing a perfect case is the key to case teaching. The case used in this paper is the CSTH model. Continuous stirred tank heater is widely used and is important system in the process and chemical industries for efficient process and good quality product[3].

Teachers are exploring an effective method of teaching in recent years. Case teaching has attracted many teachers' attention. A demo program for teaching the transformation of random variable in the context of its PDF and mean value and variance[4]. A linearized state model of a synchronous generator is introduced as an effective tool for demonstrating the value of state space control system[5]. In [6], teaching material developed with MATLAB/simulink can be successfully replaced by equivalent material developed with

Scilab/Scicos. A teaching methodology which is based on "theory and practice, basic and promotion" according to the characteristic of the teaching contents[7]. A pedagogical tool for teaching fuzzy control is presented, which develop students' practices of fuzzy logic and fuzzy control[8]. The Quadruple-Tank process is designed to illustrate many concepts in linear and nonlinear multivariable control[2]. An experiment-based approach to teaching intelligent control methodologies for students has deepened students understanding and capability to implement intelligent control strategy in real-time environment[9].

In the literatures, knowledge points are usually taught without any example or taught by different examples, which make knowledge difficult to understand. And it is hard for students to setup a whole theatrical architecture. Thus conventional teaching is not very efficient to improve creative and practical ability. To better educate undergraduates, CSTH model, which is a practical simulation platform, is selected to teaching different knowledge points.

This paper is organized as follows: In Section 2, the description of continuous stirred tank heater is presented. Section 3 presents the knowledge of instrument and PID control and cascade control and the steps of using the CSTH model to teach. Section 4 the results are concluded.

II. PROCESS DESCRIPTION

A. The Continuous Stirred Tank Heater Description[10]

The model presented in this paper comes from the Department of Chemical and Materials Engineering at the University of Alberta. In this stirred tank, hot and cold water are mixed, heated further using steam through a heating coil and drained from the tank through a long pipe. The configuration is shown in Fig 1. The CSTH is well mixed and therefore the temperature in the tank is assumed the same as the outflow temperature. The tank has a circular cross section with a volume of 8 l and height of 50 cm.

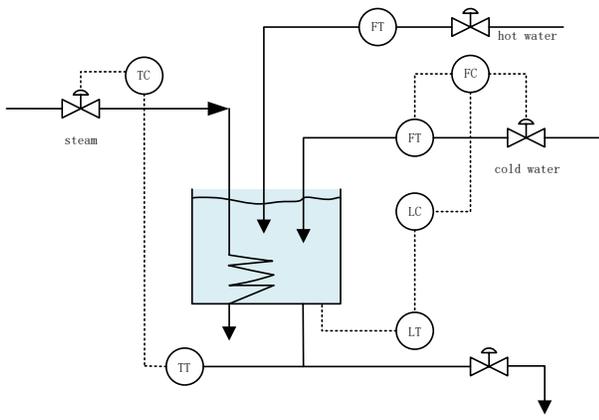


FIGURE I THE CONTINUOUS STIRRED TANK HEATER.

The cold and hot water (CW and HW) in the setup are pressurized with a pump to 60–80 psi, and the hot water boiler is heated by the university campus steam supply. The steam to the plant comes from the same central campus source. Control valves in the CSTH plant have pneumatic actuators using 3–15 psi compressed air supply, the seat and stem sets being chosen to suit the range of control. Flow instruments are orifice plates with differential pressure transmitters giving a nominal 4–20 mA output. The level instrument is also a differential pressure measurement. Finally, the temperature instrument is a type J metal sheathed thermocouple inserted into the outflow pipe with a Swagelock T-fitting.

B. Simulation Model[10]

It is difficult for some colleges to build a continuous stirred tank heater pilot plant similar to that of the University of Alberta. Therefore, simulation model teaching can be used. The simulation model of CSTH is shown in Fig 2.

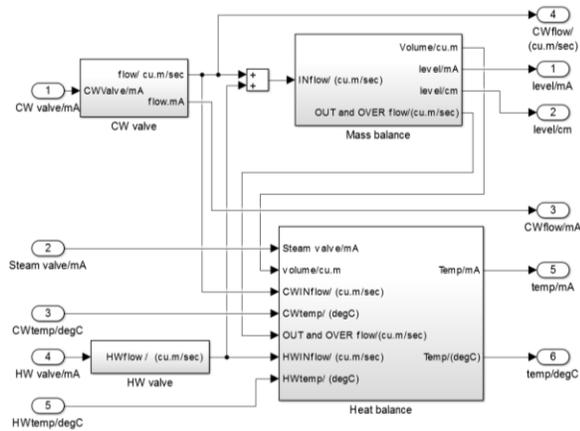


FIGURE II THE SIMULATION OF CSTH MODEL

III. CSTH BASED STUDY

The principles and simulation of the CSTH model have been introduced, and how to use CSTH to teach process control is now being discussed. Generally, CSTH can be used for theoretical modelling, PID tuning and cascade control.

A. Theoretical Modelling

Theoretical models of processes are based on conservation laws such as the balance of mass and energy which reflect movement, heat transfer, mass transfer and chemical reaction. Mass balance and energy conservation are presented in following.

1) Mass balance

The mass of water in the tank V can vary with time, and the exit flow rate is not necessarily equal to the sum of the inlet flow rates. An unsteady-state mass balance for the CSTH in Fig 1. has the form:

$$\left\{ \begin{matrix} \text{rate of accumulation} \\ \text{of mass in the tank} \end{matrix} \right\} = \left\{ \begin{matrix} \text{rate of} \\ \text{mass in} \end{matrix} \right\} - \left\{ \begin{matrix} \text{rate of} \\ \text{mass out} \end{matrix} \right\} \quad (1)$$

The mass of liquid in the tank can be expressed as the product of the water volume V and the density ρ. Consequently, the rate of mass accumulation is simply $\frac{dV(x)}{dt} \rho$, and (Eqs. 1) can be written as

$$\frac{dV(x)}{dt} \rho = f_{cw} \rho + f_{hw} \rho - f_{out}(x) \rho \quad (2)$$

where x is the level; V the volume of water; f_{hw} is the hot water flow into the tank; f_{cw} is the cold water flow into the tank; and f_{out} is the outflow from the tank. Equation can be simplified as dynamic volumetric balance because the density of water ρ, is a constant.

$$\frac{dV(x)}{dt} = f_{cw} + f_{hw} - f_{out}(x) \quad (3)$$

2) Energy conservation

The general law of energy conservation can be expressed as

$$\left\{ \begin{matrix} \text{rate of energy} \\ \text{accumulation} \end{matrix} \right\} = \left\{ \begin{matrix} \text{rate of energy in} \\ \text{by convection} \end{matrix} \right\} - \left\{ \begin{matrix} \text{rate of energy out} \\ \text{by convection} \end{matrix} \right\} + \left\{ \begin{matrix} \text{net rate of heat addition} \\ \text{to the system from} \\ \text{the surroundings} \end{matrix} \right\} + \left\{ \begin{matrix} \text{net rate of work} \\ \text{performed on the system} \\ \text{by the surroundings} \end{matrix} \right\} \quad (4)$$

The general energy balance of CSTH can be written as

$$\frac{dH}{dt} = W_{st} + h_{hw} \rho_{hw} f_{hw} + h_{cw} \rho_{cw} f_{cw} - h_{out} \rho_{out} f_{out}(x) \quad (5)$$

where H is the total enthalpy in the tank; h_{hw} the specific enthalpy of hot water feed; h_{cw} the specific enthalpy of cold water feed; h_{out} the specific enthalpy of water leaving the

tank; ρ_{cw} the density of incoming cold water; ρ_{hw} the density of incoming hot water; ρ_{out} the density of water leaving the tank; and W_{st} the heat inflow from steam.

The additional introduction of h_{out} , W_{st} , f_{out} is showed as follows:

- the specific enthalpy of water leaving the tank is

$$h_{out} = \frac{H}{\rho_{out} V c_p (T - T_{ref})} \quad (6)$$

Where c_p , and $(T - T_{ref})$ is assumed to be constant.

- The heat transfer from the steam system depends on the steam valve setting. The relationship was determined empirically from steady state running at different steam valve settings since the heat exchange area and heat transfer coefficient could not be measured. The heat balance when the Csth is in a steady state running with a cold water inflow only is:

$$W_{st} = h_{out} \rho_{out} f_{out} - h_{cw} \rho_{cw} f_{cw} \quad (7)$$

And $f_{out} = f_{cw}$ in steady state. The heat transferred at a given steam valve setting is not dependent on the temperature of the water in the tank.

- The relationship between the level in the tank and the flow through the outlet pipe is given by the equation

$$f_{out} = m \sqrt{(55 + x)} + c \quad (8)$$

where the parameters m and c can be determined by the slope and intercept of the straight line, f_{out} plotted against the constructed quantity $\sqrt{(55 + x)}$, where x is the level of the tank in cm [10, 11].

B. PID control

PID controller consists of proportional, integral and derivative, which is the most widely used industrial controller. Csth is a multivariable process, which can be controlled by PID controller when the other variables are set as constants and only one variable is left. For example, the flow rate of hot water and cold water can be set as constants so that the process conforms to the use of PID. The parallel form of the PID control algorithm is given by:

$$u(t) = K_p \left[e(t) + \frac{1}{T_i} \int_0^t e(t) dt + T_d \frac{de(t)}{dt} \right] \quad (9)$$

where K_p , T_i and T_d are, respectively, the control gain, integral time and derivative time. The functionalities are highlighted by the following.

- The proportional term:

- (1) reduces (does not eliminate) offset
 - (2) speeds up response
 - (3) for oscillatory processes, makes closed-loop process more oscillatory
- The integral term::
 - (1) eliminate offset
 - (2) may make the transient response worse
 - The derivative term:
 - (1) increasing the stability of the system
 - (2) reducing the overshoot
 - (3) improving the transient response

Effects of each of controllers K_p , K_d , and K_i on a closed-loop system are summarized in the table 1.

TABLE I. EFFECTS OF INDEPENDENT P, I, AND D TUNING

Cl response	Rise time	Over-shoot	Setting time	offset
kp	decrease	Increase	Small change	decrease
ki	decrease	Increase	increase	eliminate
kd	Small change	Decrease	decrease	Small change

When the model of process has been known, the parameter of PID should be set. The method of adjusting the parameters of the controller is named controller tuning. Controller tuning can be achieved by model-based methods and engineering controller tuning. Empirical methods are adopted in this article.

C. Cascade Control

The level control of the Csth model is somewhat more complex than the temperature control because it is affected by three factors, namely, hot water flow, cold water flow, and outlet flow. Of course, the model can be simplified, the operating for cold-water valve is set to be zero. In addition, temperature control is not necessary, so that the control of the liquid level is converted to the control of the cold water valve. The control mode is embodied in the Csth model that the chilled water valve is controlled by the controller FC, and the setpoint of the controller FC is controlled by the controller LC. Among them, LC is called the main controller, and FC is called the sub controller. This control is called cascade control. The schematic diagram of the cascade control system is shown in Fig 3.

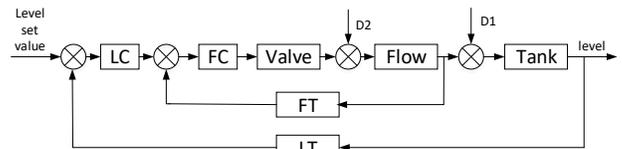


FIGURE III SCHEMATIC DIAGRAM OF CASCADE CONTROL OF Csth PROCESS

Where D1 is the disturbance of the liquid level while for D2 it is the cold-water flow.

Cascade systems contain two feedback loops :

primary loop

- a) regulate part of the process having slower dynamics
- b) calculates setpoint for the secondary loop

secondary loop

- a) regulates part of process having faster dynamics
- b) maintain secondary variable at the desired target given by primary controller

The Simulink simulation diagram of the cascade system of CSTH process is shown in Fig 4.

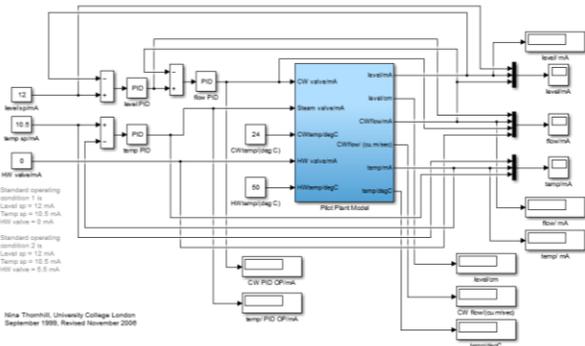


FIGURE IV SIMULINK SIMULATION DIAGRAM OF CASCADE SYSTEM OF CSTH

TABLE II. PARAMETERS VALUES FOR CASCADE CONTROL

loop	Parameter		
	Proportional gain(kp)	Integral gain(ki)	Derivative gain(kd)
primary loop	2	0.1	0
secondary loop	0.5	0.2	0

TABLE III. PARAMETERS VALUES FOR PID CONTROL

Parameter Values		
Kp	Ki	Kd
3	0.1	0

Table 1 and table 2 shows specifications of each PID value. Fig 5. shows the response of the liquid level and the cold-water valve position. Fig 6. shows the cold-water valve and hot-water valve position of the CSTH process. Fig 7. shows response of temperature and the position of steam valve.

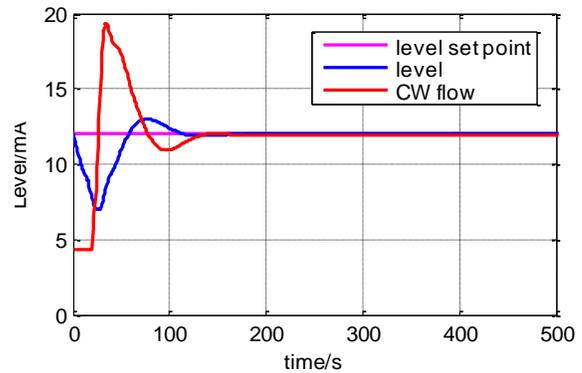


FIGURE V THE RESPONSE OF THE LIQUID LEVEL AND THE COLD-WATER VALVE POSITION

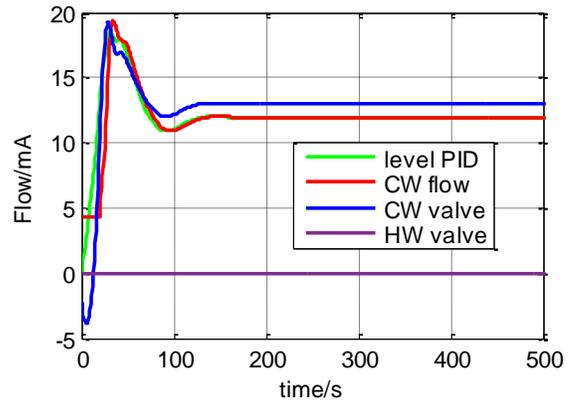


FIGURE VI THE RESPONSE OF THE COLD-WATER FLOW

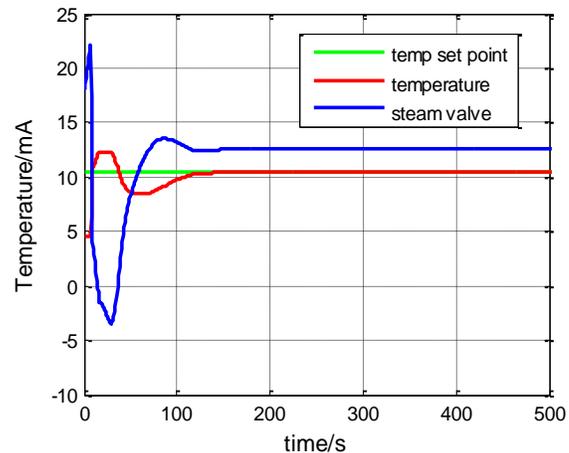


FIGURE VII THE RESPONSE OF THE TEMPERATURE

IV. CONCLUSION

In this paper, a case-based teaching method that uses the CSTH model to teach process control is presented. The CSTH is a classic industrial process model that we can get knowledge points of process control.

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